VOLUMETRIC REPORT I

J. Alexander Adams Carbon Dioxide Project Scripps Institution of Oceanography La Jolla, California 92093

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I. Introduction

During 1974 an independent check was made on the manometric calibration of the non-dispersive infrared (IR) analyzer (Applied Physics Corporation (APC) Model No. 55) located in 2317 Ritter Hall, used in this project for CO₂ analysis (reported in Manometer Report III, Guenther, 1976 a). Precise synthetic mixtures of CO₂ in N₂, O₂, and Ar were prepared and analyzed versus reference gases used in the manometric studies.

This study was suggested in 1972 when, in the course of testat Scripps two UNOR analyzers made by Maihak Corporation, Hamburg, Germany, and an URAS 1 made by Hartmann and Braun Corporation, Frankfurt, Germany, it was found that when mixtures of CO_2 in N_2 used as reference gases were compared with air, infrared index values deduced for air with the UNORs were distinctly higher than those obtained from an APC analyzer run in parallel. The difference was approximately 4 ppm for one of the UNORs and 6 ppm for the other. A close check on the performance of an URAS analyzer also being tested at the same time showed a difference on the order of 0.3 ppm from the same APC analyzer, the URAS giving, however, a lower index value than the APC. These differences are probably a result of a differential pressure broadening effect on the CO, IR absorption band when the reference gas contains a carrier gas different: from the air being analyzed. To establish this pressure broadening effect accurately for several carrier gases, the present study was undertaken.

In the experiments now to be described, seven pyrex glass flasks of approximately five liter capacity, and seven pyrex glass plenums with volumes between 1.3 and 2.3 cc, were employed to prepare synthetic mixtures of CO, in nitrogen, oxygen, and argon. The flask volumes were calibrated with water, and the plenum volumes with mercury, as described in Appendix A to this report. Ba Each plenum was filled to ambient pressure with CO2, the gas being prepared by acidifying an aqueous solution of Na₂CO₃ in a reaction vessel attached to a high vacuum system. This method insured that the CO_2 was free of other gaseous contaminants such as N_2O . The gas from an individual plenum was transferred, as described below, into a five liter flask and combined there with the selected carrier gas. While the flask temperature was controlled to within 0.01°C, the ambient pressure was measured toe the nearest Oal' mm. 1 CO, infrared ared index values, based on comparisons with Scripps primary reference gas standards, were then determined using the APC analyzer.aalyzer

The CO₂ concentrations of the gas mixtures ranged from approximately 240 to 430 ppm.

II. Experimental Procedures

A. Preparation of CO, Gas

An aqueous solution, approximately 0.56M in Na₂CO₃, was prepared in a one liter volumetric flask by weighing out 59 grams of Baker reagent anhydrous Na₂CO₃ and dissolving it in single distilled water obtained from Dr. Joris Gieskes's quartz distillery at 3255 Sverdrup Hall. Weighings were made on an Ohaus Triple Beam balance with a sensitivity of 0.5 g. Since the concentration was not critical, the Na_2CO_3 was not dried.

A solution of 1.6M H_3PO_4 was prepared by diluting 105 ml of Mallinckrodt reagent 85% H_3PO_4 solution of density 1.76 in one liter of single distilled water.

The apparatus used to prepare CO, gas is depicted in Figure 1. Fig. 1 The procedure used to fill the plenums was as follows. Stopcock S3 was closed, and all the rest of the stopcocks were opened, including those on the plenums. Stopcock S7 was then opened to the line. The system between the stopcock S3 and stopcock S8 was pumped down for three to four hours. This removed CO, adsorbed onto the glass walls and hydrocarbon joint and stopcock grease in the vacuum system. At the end of this period, the pressure of the vacuum system was measured by an Autovac Pirani-gauge conductance bridge with four individual gauge probes, and found to be less than 1.0 millitorr. Then a reaction vessel with a special funnel was attached as shown in Figure 1, and 50 ml of 0.56M Na₂CO₃ solution was pipetted via the funnel into the reaction vessel from a calibrated open ended standard pipette. A teflon coated magnetic stirring bar was inserted into the solution and the top assemblage of the reaction vessel was installed. This assemblage consisted of a special 40 ml capacity pipette closed at both ends with a 4 mm 120° curved bore stopcocks (S1 and S2), and with a 30 ml open ended chamber above. Stopcock S2 was opened, stopcock S1 was closed, and

CO, SAMPLE PREPARATION RACK





the magnetic stirrer was turned on. Thirty ml of the previously prepared 1.6M H₃PO₄ was introduced into the open ended chamber above the reaction vessel. Stopcock S9 was closed, stopcock S3 opened, and after the line pressure at Pirani-gauge G2 had fallen to 1 mm or less, stopcock S2 was closed and stopcock S1 opened to drop the H₃PO₄ into a pipette between stopcock S1 and stopcock S2. Enough additional H3PO4 solution was carefully added via the open-ended chamber to fill the pipette without allowing any bubbles of air to enter the pipette. Then stopcock S1 was closed and stopcock S2 opened slowly to let the H3PO4 drip onto the Na2CO3. About three minutes were allowed for the addition of the acid to the salt. The pressure, as measured by Pirani-gauge G2, was not allowed to rise above 2 mm during this process. Stopcock S2 was closed for a few seconds if the pressure at Pirani-gauge G2 rose too high. A spherical trap, chilled to dry ice temperature in tandem with the reaction chamber, removed the bulk of the water vapor from the CO2 stream. The CO₂ was frozen out in a concentric spherical liquid nitrogen trap beyond the water trap. After all detectable CO, had been driven from the Na2CO3 solution and the solution had frozen, stopcocks S3 and S4 were closed, and a liquid nitrogen bath was placed around U-trap Ul. Stopcock S8 was then closed, the liquid nitrogen removed from the bulb, and the CO, sublimed into U-trap Ul. This process required about fifteen minutes. Stopcock S5 was then closed and stopcock S8 opened to pull out any non-condensible gases. When

the pressure at Pirani-gauge G4 fell below 1 millitorr, a liquid nitrogen bath was placed around U-trap U2. Stopcock S8 was then closed and the liquid nitrogen bath on U-trap U1 replaced with dry ice. About twenty minutes later, with CO₂ sublimed into U-trap U2, stopcock S6 was closed and stopcock S8 opened. When the vacuum at Pirani G4 fell below 1 millitorr, stopcock S9 was opened and stopcock S8 closed. A liquid nitrogen bath was then placed around one of the long plenums. The liquid nitrogen bath on U-trap U2 was then replaced with dry ice.

After about twenty minutes, with the CO_2 now sublimed into the plenum, chilled with liquid N₂, stopcock S7 was closed and the liquid nitrogen trap taken off the plenum so that it could warm. Just as the CO_2 released from that plenum reached atmospheric pressure in the line and all of the other plenums, stopcock S7 was opened to the atmosphere so that excess CO_2 could vent. When the thawing in the plenum was complete, the plenum manifold and tube were detached from the line at the standard taper glass joint immediately below stopcock S9. The purpose of the long narrow tube from stopcock S9 to the plenum manifold was to prevent back diffusion of lab air into the plenums while allowing the plenums to be in equilibrium with atmospheric pressure. The plenum manifold was placed in a controlled temperature bath for five minutes with all plenum stopcocks still open. The bath temperature was measured with a Beckman mercury thermometer calibrated

by Walter Bryan of NORPAX against a NBS calibrated thermometer. It was controlled with a mercury contract switch that operated a 50 watt light bulb to heat the bath. Cooling was furnished by circulating water about one-half degree C cooler than the bath through a coil of copper tubing immersed in the bath. The ambient pressure was measured with a mercury wall barometer to 0.1 mm. With the apparatus at temperature equilibrium, the plenum stopcocks were closed and the temperature and pressure recorded. The plenums were immersed in liquid nitrogen for storage.

B. Preparation of Gas Mixtures

The apparatus used for gas mixture preparation is shown in Figure 2.

Carrier gas was obtained commercially as follows. Nitrogen was Liquid Carbonic Corporation's Water Pump Nitrogen, 99.98% purity. Argon was also from Liquid Carbonic. The personnel at Liquid Carbonic felt that it was probably 99.99% pure. Oxygen was Liquid Carbonic's Commercial Grade, 99.5% pure.

Stopcock S10 was opened to allow carrier gas from a high pressure steel cylinder to flow through the apparatus via an ascarite trap to insure that the carrier gas was free of CO₂. After three minutes, stopcocks S10 and S11 were opened to the vacuum line and the gas was vented through stopcock S12. A five-liter flask was imFig. 2





mersed in the controlled temperature bath and connected to the apparatus as shown. Then stopcock S11 was closed and a CO, plenum to be paired with the flask installed. Stopcock S10 was opened from the carrier gas cylinder to continue the flushing through the line. Stopcock S12 was then opened and the vacuum line as far as the flask stopcock was evacuated to less than 1 millitorr after opening stopcock Sll. Then stopcock Sll was closed. A liquid nitrogen bath was placed on U-trap U3 and the plenum stopcock was opened. After the CO, had completely sublimed from the plenum into U-trap U3 as indicated by the vacuum returning to less than 1 millitorr, stopcock S12 was closed and the flask stopcock opened. The liquid nitrogen was removed from U-trap U3 and the CO, expanded into the line and the five-liter flask. Stopcock S11 was then opened to the carrier gas line. The CO, was swept into the flask in a stream of CO2-free carrier gas. As the carrier gas filled the line, the bulb on the mercury manometer was raised to prevent CO, from being trapped in the manometer tube as the mercury was pushed down. Filling to atmospheric pressure took ten to fifteen minutes. When the flask pressure was about 1 mm less than ambient, stopcock S10 was opened to the atmosphere and the flask was equilibrated in the controlled temperature bath for ten minutes. A pressure in the system slightly less than ambient before opening to atmospheric assured that no CO, would be lost from the flask into the line upon equilibrating the system with the outside. Then

the flask stopcock was closed and pressure and temperature recorded in the same manner as with the plenum filling. Each flask so filled was allowed to stand overnight or longer to allow thorough mixing of CO_2 with the carrier gas. Flasks were stored in the dark to prevent photo-oxidation of the Apiezon "N" stopcock grease and resulting addition of CO_2 to the sample. As discussed below, each flask containing oxygen or argon was analyzed four times on the APC analyzer. Flasks containing nitrogen were analyzed six times each.

III. Results and Discussion

The plenums were paired with five-liter flasks inversely according to volume, e.g. the smallest plenum with the largest flask. This maximized the CO_2 concentration range in the prepared gas mixtures. Seven gas mixtures were obtained for each carrier gas.

Table 1 lists the index values obtained for the gas mixtures Table 1 from the APC analyzer. Listed are the index values from the 1956 Scripps index scale and the 1959 adjusted index values. The latter were used in all data interpretations. Table 2 summarizes these Table 2 numbers.

Four aliquots of gas were run against the reference gases routinely used as flask standards with adjusted index values of 319.30 and 355.44 ppm. From the CO_2-N_2 samples and additional two aliquots were run against two selected manometric standards with adjusted index values of 311.17 and 354.47 ppm. Aliquots of gas from the low manometric reference gas, adjusted index value 180.83 ppm, and from the high manometric reference gas, adjusted index value 12.55 ppm, were also analyzed with the CO_2-O_2 mixtures. Uncertainties in the index values of the reference gases and in recorder scale factor were responsible for the minor differences in computed index values of the aliquots run against flask standards and those run against manometric standards. Since the manometric standards were used only in connection with CO_2-N_2 mixtures, comparisons based on these standards were omitted from the averages listed in Table 2.

Table 3 lists the laboratory data from the volumetric synthe- Table 3 ses of gas mixtures. Table 4 lists the gas pressure data and calcu- Table 4 lated gas pressures. Table 5 lists the volumetric data and volumetric Table 5 CO, concentrations.

The volumetric concentrations were calculated according to the formula:

$$\frac{n_{1}}{n_{2}} = \frac{10^{6} v_{1} B_{2}(T_{2})}{v_{2} B_{1}(T_{1})} \qquad \frac{1 - \sqrt{1 + \frac{4P_{1} B_{1}(T_{1})}{RT_{1}}}}{1 - \sqrt{1 + \frac{4P_{2} B_{2}(T_{2})}{RT_{2}}}}$$
(1)

which derives from

$$P_{i}V_{i} = n_{i}RT_{i} + B_{i}(T_{i}) \frac{n_{i}}{V_{i}}$$
(2)

where: subscript 1 is CO2

subscript 2 is carrier gas

subscript i is either gas a constant and

n is number of moles of gas

 $\frac{n_1}{n_2}$ is CO₂ mole fraction in ppm

V is volume of gas vessel in cc

T is gas temperature in °K

R is gas constant in erg/mole-K°

- P is gas pressure in dynes/cm², obtained by setting $P = \rho gh$, where h is the observed height in cm of the column of mercury in the barometer; g is the local acceleration of gravity (979.558 cm/sec²), ρ is density of mercury in the barometer, obtained from linear interpolation of tabulated mercury densities in "Handbook of Chemistry and Physics", 43rd edition, p. 2157, Chemical Rubber Publishing Co., 1962. Handbook values were divided by 1.000027 to convert g/ml to g/cc.
- B(T) is the second density virial coefficient of gas at temperature T, obtained by quadratic interpolation of values of virials from tables in "Pressure-Volume-Temperature Relationships of Gases Virial Coefficients", Heat Division, National Bureau of Standards, Washington, D.C., 1971 (the virial at the lowest tabulated temperature higher than T plus the virials at the two highest tabulated temperatures lower than T were used in the interpolation). Units are cc/mole.

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Table 6 lists the adjusted index values and volumetric CO₂ Table 6 concentrations for the various gas mixtures.

The volumetric concentrations were plotted as functions of adjusted index values by computer (see Figure 3). The computer Fig. 3 constructed a cubic curve by least squares to run through the points. The cubic function fit the data points better than any other form of function tried. One curve was drawn for each carrier gas. They were of the form

$$V = A_0 + A_1 \cdot J + A_2 \cdot J^2 + A_3 \cdot J^3$$
(3)

where V was volumetric CO_2 concentration and J was 1959 adjusted index value. Table 7 lists the coefficients A_i for each carrier gas.

Table 7

The programs indicated that the best way to relate the changes in index values caused by changing carrier gas was to assume that the quotient:

was constant, where J_{N_2} was adjusted index value for N_2 carrier gas and J_X was adjusted index value for other carrier gases. In other words, the substitution of any carrier gas for N_2 depressed the adjusted index value by a constant factor independent of CO_2 -concentration.



Figure 3. Calibration curves for CO_2 in various carrier gases. Volumetric CO_2 concentration is plotted vs. 1959 Adjusted Index value. The curve furthest to the right is from CO_2-N_2 mixtures; the middle curve is from CO_2-O_2 mixtures; and the curve furthest to the left is from CO_2-Ar mixtures.

Table 8 lists the values of this factor for various CO_2 mole fractions, where J_{N_2} , J_{Ar} , and J_{O_2} were computed from equation (3) using the coefficients of Table 7.

The average depression in adjusted index value caused by replacing N₂ with Ar was 8.24% with an absolute standard deviation (σ) of 0.26%. Adjusted index values for 0₂-CO₂ averaged 5.26% lower than those for N₂-CO₂ with an absolute standard deviation of 0.18%.

If it is assumed that these depressions in adjusted index values are linear with mole fraction of the non-N₂ carrier gas, the depression in index value caused by replacing N₂ with air, if air is 0.934% Ar and 20.946% O₂, can be calculated by the formula

$$\frac{J_{N_2} - J_{Air}}{J_{N_2}} = 0.00934 \cdot 0.0824 + .20946 \cdot 0.0526 = 1.18\%$$

An independent method of measuring the depression in 1959 adjusted index value caused by the presence of O_2 and Ar in air was performed by P. R. Guenther of the Scripps laboratory research group using a constant volume manometer in 2317 Ritter Hall. As opposed to the volumetric method of synthesizing gas mixtures and determining the CO_2 concentration on the APC analyzer, the manometric method was to analyze a gas mixture from a compressed gas cylinder by removing an aliquot, measuring its volume, pressure and temperature, and extracting the CO_2 and measuring its volume, pressure and temperature. These gas mixtures were also run extensively on the APC analyzer. Manometric analyses done on CO_2-N_2 and

. Table 8

CO₂-air mixtures indicated a lowering of the adjusted index value on the APC analyzer of 1.20% (see Manometric Report III, Guenther, 1976). Thus the air corrections measured by the two methods agree quite well.

Guenther also analyzed some artificial air mixtures, containing about 330 ppm CO_2 , prepared by Liquid Carbonic Corporation and certified at 20% O_2 in N_2 . He obtained O_2 mole fractions on the artificial air by a paramagnetic comparison with real air with its precisely know O_2 mole fraction. He normalized the measured O_2 -caused depression in 1959 adjusted index value for artificial air to real air O_2 -mole fraction. The argon caused depression, deduced from the difference in depression between artificial and real air, agreed very closely with the direct volumetric determination.

It is concluded that the adjusted index value obtained for an airs sample with the Scripps APC analyzer in 2317 Ritter Hall should be corrected by adding 1.2% to its value to obtain the adjusted index value the APC analyzer would yield if only N₂ were present in the sample as carrier gas (called virtual adjusted index by Guenther). Both this virtual adjusted index and the actually obtained adjusted index value can be converted to CO_2 mole fraction using the relationship between adjusted index value and mole fraction for $CO_2 - N_2$ mixtures. The difference combetween the two mole fractions obtained is the error in CO_2 concentration read by the APC analyzer which results from comparing air samples to $CO_2 - N_2$ standards. The contribution to

this error of 0, and Ar in the air can also be calculated from the CO2-O2 and CO2-Ar mixture comparisons with CO2-N2 mixtures in the volumetric experiment (Table 7) and the manometric artificial air analyses. Table 9 lists the errors in CO₂ mole fraction caused by the different air carrier gases at 1959 adjusted index values of 310, 320, and 330 ppm. The results of both volumetric and manometric measurements are included.

Supplemental Experiments IV.

A. Influence of N₂O on the Infrared CO₂ Analyzer

An experiment was conducted to determine the effect of N_20 on the response of the APC infrared analyzer to CO_2 . The plenums were filled to ambient pressure directly from a cylinder of medical grade (99.9%) N₂O from L & V Industrial Supply Inc., Encinitas, California, on the vacuum line used for CO2-N2 mixtures. They were then placed in the controlled temperature bath described earlier. After waiting for five minutes to achieve temperature equilibrium, the plenums were placed in the liquid N, bath for storage described earlier. The N₂O was not purified because it was assumed that the APC analyzer would be so insensitive to N20 that minor impurities would not detectably affect the APC analyzer's response to N,0.

After warming a given plenum, the N₂O in it was swept into a five liter flask with N2 gas according to the procedure for CO_2 in N₂ described above. The resulting mixture was then analyzed on the APC analyzer. A vacuum pen trace was first obtained and

Table 9

the displacement from the vacuum trace caused by N_2^0 noted when the $N_2^0-N_2$ mixture was put into the analyzer cell. The laboratory data are recorded in Table 10. The lowest concentration mixture, 240 ppm of N_2^0 , caused a barely readable displacement of 0.2 scale divisions, and the highest concentration mixture, 430 ppm N_2^0 , caused a displacement of 0.3 scale divisions. At the given span setting, $C0_2-N_2$ mixtures of similar concentration caused displacements of 60 and 90 scale divisions, respectively. These were the low manometric standard, cylinder No. 2408, manometric $C0_2$ concentration 196.90 ppm, and the high manometric standard, cylinder No. 34316, manometric $C0_2$ concentration 472.97 ppm. Therefore, the analyzer was approximately 300 times as sensitive to $C0_2$ as to N_2^0 at these low concentrations.

Another experiment was run with higher N_2^{0} concentrations. Medical grade N_2^{0} was expended into each of three previously evacuated 5-liter flasks to a specific pressure. The flask stopcocks were closed and the connecting vacuum line was pumped to less than 1 millitorr, then filled with a CO_2-N_2 reference gas from a high pressure cylinder to a pressure greater than that of the N_2^{0} in the flask. Thus when the flask stopcock was opened, no N_2^{0} was lost into the vacuum line. With the stopcock open the flask was filled to ambient pressure with the CO_2-N_2 mixture. The result was a CO_2-N_2 sample considerably contaminated with N_2^{0} . Pressures were measured on a mercury column read with a meter stick. Table 11 lists the results. The N_2^{0} pressures of the mixtures were 5.1 mm Hg,

Table 10

Table 11

9.3 mm Hg, and 18.1 mm Hg. The reference gas used for the first two mixtures were from cylinder No. 6071 with an adjusted index value of 318.40 ppm CO_2 . For the third mixture the reference gas came from cylinder No. 4285 with an adjusted index value of 349.90 ppm CO_2 . All the CO_2 adjusted index values were converted to mole fractions using the cubic relationship, in equation (3), for CO_2-N_2 mixtures with the coefficients listed in Table 7. The CO_2 mole fractions were corrected for the dilution caused by the added N₂O by the relationship

Total pressure - N_2^0 pressure mole fraction(corrected) = $CO_2 N_2$ mole fraction x co by normalized in N_2^0 were computed to by 6696, 12208, and 23756 ppm by the ratios of N_2^0 pressure to ambient pressure. The response ratios found by infrared analysis were approximately 550, 740, and 950 ppm N_2^0 /ppm CO_2 , respectively. Therefore, the N_2^0 response of the APC analyzer is not linear with CO_2 response but decreases with increasing concentration of N_2^0 . This result is consistent with finding a ratio of 300 at low N_2^0 concentration. It is concluded that normal air, which contains about 0.3 ppm N_2O_2 , can be analyzed for CO_2 by the infrared method without making any correction for the infrared absorption of N_2^0 , since air N_2^0 would cause a pen displacement on the recorder equivalent to approximately 0.001 ppm CO_2 .

B. Influence of H₂O on the Infrared CO₂ Analyzer

The influence of water vapor on APC analyzer response was also determined. About 5 cc of single distilled water was injected into four previously evacuated 5-liter flasks and the flasks brought to ambient pressure with reference gases as described above. Two flasks were filled with reference gas from cylinder No. 6071 and two were filled from cylinder No. 4285. The samples were run on the APC analyzer with and without dry ice on the cold trap on the line leading to the analyzer cell. The water vapor was assumed to be in equilibrium with liquid water at the ambient temperature. The vapor pressure was calculated from data listed in the Handbook of Chemistry and Physics, 43rd edition, p. 2361-2364, Chemical Rubber Publishing Company, 1962. Tables 10 and 12 list the results of this experiment.

As with the N_2^0 sensitivity experiment, adjusted index values were converted to mole fractions by the volumetric cubic relationship, and mole fractions were corrected for dilution by the added interfering gas, in this case, water vapor. At the laboratory ambient temperature of 22.0°C, the H₂0 concentration (the ratio of vapor pressure of liquid water to ambient pressure) was approximately 26300 ppm. The average ppm H₂0/ppm CO₂ response ratio was found to be 660. When 319 ppm CO₂ was present, the ratio was 680; when 350 ppm CO₂ was present the ratio was 630.

Table 12

It can concluded that water vapor, as well as N₂O, does not interfere significantly with the analyzer during routine air CO₂ measurements. Since water vapor in equilibrium with water ice at dry ice temperature is about 0.7 ppm, and the response ratio for water was 660 to 1, the recorder pen displacement caused by water is equivalent to approximately 0.001 ppm CO₂, provided that the dry ice trap is removing all water vapor above the equilibrium vapor pressure.

C. Manometer Volume Calibration

The 4 cc chamber in the manometric system in Room 2317 Ritter Hall was calibrated with volume-calibrated CO_2 plenums used in the experiments described above. The largest and smallest plenums were used. At first the same procedure was used for filling them with CO_2 as previously described. However, discrepancies occurred between results obtained from the small and large plenums. The large plenum results indicated a larger volume for the 4 cc chamber. The liquid N₂ bath was placed on the larger plenum to trap purified CO_2 prior to subliming it into the plenums and plenum manifold. If the purification described above had failed to remove all of the water vapor, it could possibly have collected in the large plenum with the CO_2 , remained condensed on the dry ice in the large plenum while the CO_2 filled the manifold and plenums, and evaporated after all CO_2 ice was gone, but remained in the large plenum because of slow diffusion through CO_2 at 1 atmosphere pressure in a long, narrow tube. This water vapor would have been removed in the dry ice-covered U-traps used by Guenther in transferring the CO₂ from the plenum to the 4 cc chamber. The result would have been less gas in the 4 cc chamber than calculated and a consequent lower pressure reading on the gas in the 4 cc chamber than should have been obtained, resulting in an erroneously large volume.

This was consistent with a finding that the samples contained residual water vapor by the following test. The CO₂ was transferred from the large plenum to a U-trap at liquid nitrogen temperature with a dry ice trap on the plenum. After transfer, the manifold to which the plenum was attached was closed to the U-trap and the dry ice removed from the plenum. The pressure in the manifold then rose from less than 1 millitorr to 7 or 8 millitorr. The manifold volume was estimated to be about 200 times the plenum volume. Therefore, the previous water vapor pressure in the plenum was evidently about 1.5 mm, or 2 parts per thousand, an unacceptable contamination. This phenomenon was not noted when the small plenum was attached to the manifold. To eliminate water vapor from the CO₂ samples, four alterations were made in the procedure for filling the CO₂ plenum:

(1) A glass flask consisting of a closed 20 mm diameter tube 10 cm long with an attached glass stopcock was placed on the vacuum line next to stopcock S8 (see Figure 1). CO₂ could be distilled back and fourth between flask and U-trap U2 as many times as necessary to remove residual water. A liquid N_2 bath was placed on the flask, the flask stopcock opened, stopcock S8 closed, and liquid N_2 on the trap U2 replaced with dry ice. After about 1 1/2 hours, the flask stopcock was closed, the dry ice taken off trap U2, stopcock S8 opened, and a heat gun played on trap U2 to warm it up and drive off adsorbed water. Then a liquid N_2 bath was place on U-trap U2, stopcock S8 closed, a dry ice trap placed on the flask, and the flask stopcock opened. This transfer took about 1 hour. Then stopcock S7 was closed, stopcock S8 opened, the dry ice taken off the flask and a heat gun played on the flask. Stopcock S7 was then opened from U-trap U2 to stopcock S8. This process was repeated twice.

(2) A large vial was put onto the plenum manifold initially to trap the CO₂. This vial consisted of a closed 12 mm tube 20 cm long with attached glass stopcock (see Figure 1). The CO₂ was then sublimed into this vial from the line, and from the vial into the volumecalibrated plenums and connecting manifold. Any water in the vial thus tended to remain there and not enter the calibrated plenum, just as previously the water remained in the large plenum.

(3) CO_2 gas was introduced directly from a cylinder of commercial grade CO_2 gas purchased from the Matheson Company, Inc., 99.5% pure, rather than derived from a Na_2CO_3 solution. This eliminated liquid water from the vacuum system (see Figure 1). By setting the CO_2 flow from the cylinder such that the pressure, registered on Pirani-gauge

G2 was 0.5 mm, sufficient CO_2 for the experiment was frozen in about 10 minutes into the liquid N₂ concentric spherical trap. Then stopcocks S3 and S4 were closed and the process described above for Na₂CO₃-derived CO₂ was repeated, with the additional glass vessels and procedures described above in items (1) and (2) of this section.

(4) The bulb trap immersed in the dry ice slurry between stopcocks S3 and S4 was replaced with a simple thimble trap filled with glass wool. This removed a greater proportion of the water vapor from the CO₂ stream than the spherical trap.

These modifications in the procedure seemed to remove all water from the CO_2 , as no further evidence came to light of water vapor in the CO_2 transferred into the 4 cc chamber of the manometer. Also, no further discrepancies between 4 cc manometer chamber volume determinations measured by CO_2 from different plenums were found.

The initial calibrations of the 4 cc chamber were not included in Manometer Report IV. Further measurements, after eliminating the water vapor problem, are reported in Manometer Report IV.

Water in the CO₂ plenums may explain some of the scatter in the points about the calibration curves for each carrier gas, (figure 3, Table 6).-----

D. Calibration of the Wall Barometer in 2328 Ritter Hall

On 15 June 1976 the wall barometer from which pressures were obtained in the foregoing experiments was calibrated with the cathetometer and columns No. 2 and 4 in the manometer in 2317 Ritter Hall. (For definition of column numbers, see Manometer Report I) Atmospheric pressure was introduced to column No. 4 in the manometer, with column No. 2 connected to the vacuum pump. The doors to the laboratory rooms were opened to the hall in insure pressure equilibration. A pair of readings was taken by Mr. Peter Guenther on the level of mercury on column No. 4 (low level), followed by a pair of readings on column No. 2 (high level, vacuum), followed by readings on column No. 4, then No. 2, then No. 4. The pairs of readings were averaged together, and differences were calculated for each set of adjacent readings on columns No. 2 and No. 4. Temperatures of the case were read during readings of column No. 4.

While readings were being taken on the mercury level in column No. 4, the pressure was taken in 2328 on the wall barometer by Adams, along with the temperature of the mercury column from a thermometer attached to the barometer. The column heights read in 2328 were normalized to the temperature of the manometer.case by multiplying the wall barometer column height by the ratio of mercury density at temperature of 2328 to mercury density at manometer case temperature. This resulted in average pressures of 762.40 mm by the cathetometer, and 762.42 mm by the wall barometer. These values were well within experimental error of each other, since the wall barometer is readable to only 0.1 mm.

Table 13 lists the data obtained in this experiment. Table 13

Cylinde Primary	r-Number <u>High Span</u>	Scale Difference Between Reference Gases	Index Difference Between Reference Gases	Flask Number	Scale Difference Between Sample and Primary	Index Difference Between Sample and Primary	Sample Index	Sample Adjusted Index
			<u>co</u> 2-	N2 MIXTURE	S			
4297	3755	35.9 35.9						
				C-8	-82.0	-67.70	250.19	236.79
	11 M	1.70		C-8	-82.1	-67.78	250.11	236.69
	61-10	4419		C-7	-46.2	-38.14	279.75	272.81
	0.1	~		C-7	-46.4	-38.31	279.58	272.60
	Kht	25		C-10	-10.7	-8.83	309.06	308.52
				C-10	-10.8	-8.92	308.97	308.41
				C-5	10.1	8.34	326.23	329.45
				C-5	10.1	8.34	326.23	329.45
				C-3	26.8	22.13	340.02	346.25
				C-3	26.8	22.13	.340.02	346.25
				C-9	65.6	54.16	372.05	385.28
				C-9	65.6	54.16	372.05	385.28
4297	3755	35.9 36.0						
	Average of 'fo	our 35.925	29.66	Rec	corder Scale Fa	actor = 0.82561	. ppm/scale	division '

Primary Index Value = 317.89 ppm

Cylind Primary	eruNumber High Span	Scale Difference Between Reference Gases	Index Difference Between Reference Gases	Flask Number	Scale Difference Between Sample and Primary	Index Difference Between Sample and Primary	Sample Index	Sample Adjusted Index
			<u>co</u> 2-	N2 MIXTURE	S		-	
4297	3755	29.5						
				C-11	84.9	85.72	403.61	423.74
				C-11	84.7	85.52	403.41	423.50
				C-8	-67.1	-67.75	250.14	236.72
				C-8	-67.1	-67.75	250.14	236.72
	11 1111 -711			C-7	-37.7	-38.07	279.82	272.89
	16 May 14			C-7	-37.8	-38.17	279.72	272.77
	0			C-10	-8.8	-8.89	309.00	308.45
				C-10	-8.8	-8.89	309.00	308.45
				C-5	8.1	-8.18	326.07	329.25
				C-5	8.2	-8.28	326.17	329.37
				C-3	21.8	22.01	339.90	346.11
				C-3	21.7	21.91	339.80	345.98
				C-9	53.7	54.22	372.11	385.36
				C-9	53.7	54.22	372.11	385.36
				C-11	84.7	85.52	403.41	423.50
				C-11	84.7	85.52	403.41	423.50
4297 :	3755	29.2 29.4		-				
	Average of four	r 29.375	29.66	Rec	order Scale Fa	actor = 1.00970) ppm/scale	division

Primary Index Value = 317.89 ppm

TABLE 1.	Index and	Adjusted	Index	Values	for	Volumetric	Gas	Samples	
			and the second se	and the second se					

Cylinde Primary	er Number <u>High Span</u>	Scale Difference Between Reference Gases	Index Difference Between Reference Gases	Flask <u>Number</u>	Scale Difference Between Sample and Primary	Index Difference Between Sample and Primary	Sample Index	Sample Adjusted Index
			<u>co</u> 2-	N ₂ MIXTURE	S			
6078*	10069*	34.7 34.8						
				C-8	-60.4	-61.62	249.61	236.08
				C-8	-60.6	-61.83	249.40	235.82
				C-7	-31.2	-31.83	279.40	272.38
				C-7	-31.2	-31.83	279.40	272.38
	DIN	111174		C-10	-2.3	-2.35	308.88	308.31
	\$11°	ing 17		C-10	-2.2	-2.24	308.99	308.44
		~		C-5	14.7	15.00	326.23	329.45
				C-5	14.7	15.00	326.23	329.45
				C-3	28.2	28.77	340.00	346.23
				C-3	28.2	28.77	340.00	346.23
				C-9	59.9	61.11	372.34	385.64
			1	C-9	59.8	61.01	372.24	385.52
				C-11	90.7	92.54	403.77	423.94
				C-11	90.8	92.64	403.87	424.06
6078*	10069*	35.0 34.8						
	Average of fo	our 34.825	35.53	Red	corder Scale Fa	actor = 1.02024	ppm/scale	division
				Pr	Lmary Index Val	ue = 311.23 pp	m	

*Manometric Reference Gases

Cylin Primary	der Number <u>High Span</u>	Scale Difference Between Reference Gases	Index Difference Between Reference Gases	Flask Number	Scale Difference Between Sample and Primary	Index Difference Between Sample and Primary	Sample Index	Sample Adjusted Index
			<u>co</u> 2-	Ar MIXTURE	<u>IS</u>			
4297	3755	26.1 25.9						
				C-8	-74.8	-85.00	232.89	215.70
				C-8	-74.8	-85.00	232.89	215.70
				C-7	-50.2	-57.05	260.84	249.76
	31 May 14			C-7	-50.2	-57.05	260.84	249.76
)	•		C-10	-26.4	-30.00	287.89	282.73
				C-10	-26.4	-30.00	287.89	282.73
				C-5	-12.8	-14.55	303.34	301.55
				C-5	-12.8	-14.55	303.34	301.55
				C-3	-1.3	1.48	316.41	317.48
				C-3	-1.3	-1.48	316.41	317.48
				C-9	. 25.7	29.21	347.10	354.88
				C-9	25.7	29.21	347.10	354.88
			· · · ·	C-11	50.9	57,84	375.73	389.77
				C-11	50.9	57.84	375.73	389.77
4297	3755	26.2						
	Average of four	26.10	29.66	Rec	corder Scale Fa	actor = 1.13640	ppm/scale	division

Primary Index Value = 317.89 ppm

. 1

Cylinde Primary	er Number High Span	Scale Difference Between Reference Gases	Index Difference Between Reference Gases	Flask Number	Scale Difference Between Sample and Primary	Index Difference Between Sample and Primary	Sample Index	Sample Adjusted Index
			<u>co</u> 2-	Ar MIXTURE	<u>s</u>			
4297	3755	26.2						
				C-8	-74.8	-84.68	233.21	216.09
				C-8	-74.8	-84.68	233.21	216.09
				C-7	-50.2	-56.83	261.06	250.03
				C-7	-50.2	-56.83	261.06	250.03
	21 Man	14		C-10	-26.5	-30.00	287.89	282.73
	DI & invol	//		C-10	-26.6	-30.11	287.78	282.59
	0	14		C-5	-12.7	-14.38	303.51	301.76
				C-5	-12.7	-14.38	303.51	301.76
				C-3	1.4	1.58	316.31	317.36
			3.	C-3	-1.4	-1.58	316.31	317.36
				C-9	25.8	29.21	347.10	354.88
				C-9	25.7	29.09	346.98	354.73
				C-11	50.9	57.62	375.51	389.50
				C-11	50.9	57.62	375.51	389.50
4297	3755	26.2 26.2						
	Average of fou	r 26.20	29.66	Rec	corder Scale Fa	actor = 1.13206	ppm/scale	division

Primary Index Value = 317.89 ppm

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TABLE I. Index and Adjusted Index Values for Volumetric Gas Samples

Cylinder Primary	Number <u>High Span</u>	Scale Difference Between Reference Gases	Index Difference Between Reference Gases	Flask Number	Scale Difference Between Sample and Primary	Index Difference Between Sample and Primary	Sample Index	Sample Adjusted Index
			<u>co</u> 2-c	2 MIXTURE	S			
4297	3755	22.9						
		22.8						
				35316*	84.1	109.16	427.05	452.31
				35316*	84.2	109.29	427.18	452.47
	105	1. 24		2408†	-87.0	-112.93	204.98	181.69
	103	une 17		2408†	-87.1	-113.06	204.83	181.51
		1 .		C-8	-60.2	-78.14	239.75	224.06
				C-8	-60.1	-78.01	239.88	224.22
				C-7	-38.1	-49.45	268.44	259.02
				C-7	-38.1	-49.45	268.44	259.02
				C-10	-16.6	-21.55	296.34	293.02
				C-10	-16.6	-21.55	296.34	293.02
				C-5	-4.0	-5.19	312.70	312.96
				C-5	-4.1	-5.32	312.57	312.80

*High-CO₂ manometric CO₂-N₂ compressed gas cylinder +Low-CO₂ manometric CO₂-N₂ compressed gas cylinder

Cylinder Number Primary High Spa	Scale Difference Between Reference n Gases	Index Difference Between Reference Gases	Flask Number	Scale Difference Between Sample and Primary	Index Difference Between Sample and Primary	Sample Index	Sample Adjusted Index
		<u></u>	-0_2 MIXTURE	5			
			C-3	6.1	7.92	325.81	328,94
			C-3	6.1	7.92	325.81	328.94
	(un	entel	C-9	29.8	38.68	356.57	366.42
	l'o sunerg	cont a)	C-9	29.8	38.68	356.57	366.42
			C-11	5313	69.18	387.07	403.57
			C-11	531.3	69.18	387.07	403.57
			35316*	83.8	108.77	426.66	451.83
			35316*	83.8	108.77	426.66	451.83
			2408†	-87.2	-113.19	204.70	181.35
			2408†	-87.3	-113.32	204.57	181.19
4297 3755	22.9						
	22.8						
Averagecof	four 22.85	29.66	Rec	order Scale Fa	actor = 1.29803	B ppm/scale	division
			Pris	mary Index Val	ue = 317 89 pr	m	

*High-CO₂ manometric CO_2-N_2 compressed gas cylinder *Low-CO₂ manometric CO_2-N_2 compressed gas cylinder

Cylinder Primary	Number High Span	Scale Difference Between Reference Gases	Index Difference Between Reference Gases	Flask Number	Difference Between Sample and Primary	Index Difference Between Sample and Primary	Sample Index	Sample Adjusted Index
			<u>co</u> 2-	02 MIXTURE	S			
4297	3755	22.9 22.8						
				35316*	84.1	108.93	426.82	452.07
				35316*	84.0	108.80	426.69	451.87
				2408†	-87.1	-112.81	205.08	181.81
				2408†	-87.2	-112.94	204.95	181.66
		70.		C-8	-60.1	-77.84	240.05	224.43
	10	June !!		C-8	-60.3	-78.10	239.79	224.11
				C-7	-38.3	-49.61	268.28	258.83
				C-7	-38.3	-49.61	268.28	258.83
				C-10	-16.7	-21.63	296.26	292.93
				C-10	-16.8	-21.76	296.13	292.77
				C-5	-4.2	-5.44	312.45	312.66
				C-5	-4.2	-5.44	312.45	312.66

*High-CO₂ manometric CO_2-N_2 compressed gas cylinder *Low-CO₂ manometric CO_2-N_2 compressed gas cylinder

Cylind Primary	er Number High Span	Scale Difference Between Reference Gases	Index Difference Between Reference Gases	Flask <u>Number</u>	Scale Difference Between Sample and Primary	Index Difference Between Sample and Primary	Sample Index	Sample Adjusted Index
			<u>co</u> 2-	02 MIXTURES				
4297	3755	(10 June7 23.2 22.7	Y Contra)	C-3 C-9 C-9 C-11 C-11 35316* 35316* 2408† 2408†	6.1 6.0 29.8 29.8 53.2 53.2 53.2 83.9 83.9 -87.1 -87.2	7.90 7.77 38.60 38.60 68.90 68.90 108.67 108.67 -112.81 -112.94	325.79 325.66 356.49 356.49 386.79 386.79 426.56 426.56 205.08 204.95	328.91 328.75 366.32 366.32 403.25 403.25 403.25 451.71 451.71 181.81 181.66
	Average of four	22.90	29.66	Reco	rder Scale Fa	tor = 1.29520) ppm/scale	division
	35316 35416	the first- C_{Z}^{0}	anometric sta	Prin ndard. uard.	ary Index Val	.ue = 317.89 pp	m	
*	High-CO ₂ manome	etric CO ₂ -N ₂ c	compressed gas	cylinder ylinder				

CO2-N2 MIXTURES

		Adjusted		Average
	Index	Index	Average	Adjusted
Flask No.	Values	Values	Index	Index
C-8	250.19	236.79		
	250.11	236.69		
	250.14	236.72		
	250.14	236.72		
	249.61*	236.08*		
	249.40*	235.82*	250.14	236.72
C-7	279.75	272.81		
	279.58	272.60		
	279.82	272.89		
	279.72	272.77		
	279.40*	272.38*		
	279.40*	272.38*	279.72	272.77
C-10	309.06	308.52		
	308.97	308.41		
	309.00	308.45		
	309.00	308.45	4	
	308.88*	308.31*		
	308.99*	308.44*	309.01	308.46
C-5	326.23	329.45		
	326.23	329.45		
	326.07	329.25		
	326.17	329.37		
	326,23*	329.45*		
	326.23*	329.45*	326.18	329.39
C-3	340.02	346.25		
	340.02	346.25		
	339.90	346.11		
	339.80	345.98		
	340.00*	346.23*		
	340.00*	346.23*	339.94	346.15

*Referred to values based on comparison with Manometric Standards not used in average.
TABLE 2.Summary of Index and AdjustedIndex Values for Volumetric Gas Samples

CO2-N2 MIXTURES

	Index	Adjusted Index	Average	Average Adjusted
Flask No.	Values	Values	Index	Index
C-9	372.05	385.28		
	372.05	385.28		
	372.11	385.36		
	372.11	385.36		
	372.34*	385.64*		
•	372.24*	385.52*	372.08	385.32
C-11	403.61	423.74		
	403.41	423.50		
	403.41	423.50		
	403.41	423.50		
	403.77*	423.94*		
	403.87*	424.06*	403.46	423.56

*Referred to Manometric Standards - not used in average.

TABLE 2.Summary of Index and AdjustedIndex Values for Volumetric Gas Samples

CO2-Ar MIXTURES

		Adjusted		Average
	Index	Index	Average	Adjusted
Flask No.	Values	Values	Index	Index
C-8	232.89	215.70	Section 2	
	232.89	215.70		
	233.21	216.09		
	233.21	216.09	233.05	215.90
C-7	260.84	249.76		
	260.84	249.76		
	261.06	250.03		
	261.06	250.03	260.95	249.90
C-10	287.89	282.73		
	287.89	282.73		
	287.89	282.73		
	287.78	282.59	287.86	282.70
C-5	303.34	301.55		
	303.34	301.55		
	303.51	301.76		
	303.51	301.76	303.42	301.65
C-3	316.41	317.48		
	316.41	317.48		
	316.31	317.36		
	316.31	317.36	316.36	317.42
C-9	347.10	354.88		
	347.10	354.88		
	347.10	354.88		
	346.98	354.73	347.07	354.84
C-11	375.73	389.77		
	375.73	389.77		
	375.51	389.50		
	375.51	389.50	375.62	389.63

TABLE 2.Summary of Index and AdjustedIndex Values for Volumetric Gas Samples

CO2-02 MIXTURES

		Adjusted		Average
	Index	Index	Average	Adjusted
Flask No.	Values	Values	Index	Index
C-8	239.75	224.06		
	239.88	224.22		
	240.05	224.43		
	239.79	224.11	239.87	224.21
C-7	268.44	259.02		
	268.44	259.02		
	268.28	258.83		
	268.28	258.83	268.36	258.93
C-10	296.34	293.02		
	296.34	293.02		
	296.26	292.93		
	296.13	292.77	296.27	292.94
C-5	312.70	312.96		
	312.57	312.80	ale .	
	312.45	312.66		
	312.45	312.66	312.54	312.77
C-3	325.81	328.94		
	325.81	328.94		
	325.79	328,91		
	325.66	328.75	325.77	328.89
C-9	356.57	366.42		
	356.57	366.42		
	356.49	366.32		
	356.49	366.32	356.53	366.37
C-11	387.07	403.57		
	387.07	403.57		
	386.79	403.25		
	386.79	403.25	386.93	403.42

TABLE 3. Gas State Data

<u>co</u>2

Gas Mixtures

Plenum	Volume	Date	Flask	Volume	Barometer Reading mm	Barometer	Gas Temp °C
					iteretarity and	U	acmp. 0
	1 0070	CO N	Mixtures				
P-1	1.2978	<u><u><u> </u></u></u>	ILLAC GL CO				
	1 1/10		Plenums	Variable	761.8	20.7	20.72
P-2	1.4619	14 MAY 74	4 C-8	5389.1	761.8	20.2	20.74
	1 (0(0	14 MAY 74	4 C-7	5350.2	762.7	20.0	20.74
P-3	1.6360	14 MAY 74	4 C-10	5329.8	762.1	20.6	20.73
		14 MAY 74	4 C-5	5320.2	762.3	20.6	20.73
P-4	1.7457	14 MAY 74	4 C-3	5315.0	762.1	20.1	20.75
		14 MAY 74	4 C-9	5237.2	762.8	20.5	20.76
P-5	1.8359	14 MAY 74	4 C-11	5224.1	762.0	20.2	20.74
P-6	2.0367	. <u>CO</u> 2-A	r <u>Mixtures</u>				
			Plenums	Variable ·	763.2	21.8	20.74
P-7	2.2733	28 MAY 74	4 C-8	5389.1	763.9	19.7	20.76
		28 MAY 74	4 C-7	5350.2	763.1	20.7	20.77
		28 MAY 74	4 C-10	5329.8	764.1	20.3	20.77
		28 MAY 74	4 C-5	5320.2	764.1	19.7	20.76
	•	28 MAY 74	4 C-3	5315.0	763.7	20.6	20.76
		28 MAY 7	4 C-9	5237.2	764.0	20.5	20.77
		28 MAY 7	4 C-11	5224.1	763.4	20.6	20.78
		<u>co20</u>	Mixtures				
			Plenums	Variable	760.0	20.7	20.75
		6 JUN 7	4 C-8	5389.1	758.5	20.3	20.75
		6 JUN 7	4 C-7	5350.2	758.5	20.3	20.74
		6 JUN 7	4 C-10	5329.8	758.3	20.9	20.76
		6 JUN 7	4 C-5	5320.2	757.8	20.4	20.76
		6 JUN 7	4 C-3	5315.0	757.9	20.6	20.76
		6 JUN 7	4 C-9	5237.2	757.9	20.3	20.75
		6 JUN 7	4 C-11	5224.1	758.0	20.8	20.76

TABLE 4. Gas Pressure Calculations

Fi Flask No. ner	Barometer Temperature °C	Hg Density _g/ml	Hg Density _g/cc	Hg Column Height mm	Pressure ₂ Dynes/cm
CO2-N2 Mixtur	es				
Plenums	20.7 .	13.5445	13.5441	761.8	1.01070:106
C-8	20.2	13.5457	13.5453	761.8	1.01079:106
C-7	20.0	13.5462	13.5458	762.7	1.01202.106
C-10	20.6	13.5448	13.5444	762.1	1.01112:106
C-5	20.6	13.5448	13.5444	762.3	1.01138:106
C-3	20.1	13.5460	13.5456	762.1	1.01121:10 ⁶
C-9	20.5	13.5450	13.5446	762.8	1.01206:106
C-11	20.2	13.5457	13.5453	762.0	1.01106.106
CO2-Ar Mixtur	es				
Plenums	21.8	13.5418	13,5414	763.2	1.01236.106
C-8	19.7	13.5470	13.5466	763.9	1.01367.106
C-7	20.7	13,5445	13.5441	763.1	1.01243.106
C-10	20.3	13,5455	13.5451	764.1	1.01383.106
C-5	19.7	13.5470	13.5466	764.1	1.01394.106
C-3	20.6	13,5448	13.5444	763.7	1.01324.106
C-9	20.5	13,5450	13.5446	764.0	1.01366.106
C-11	20.6	13.5448	13.5444	763.4	1.01284.106

Local acceleration of gravity = 979.558 cm/sec^2

lg/cc = lg/ml + 1.000027

TABLE 4. Gas Pressure Calculations

.T ..

Flask CoNo.ingr	Barometer Temperature °C	Hg Density g/ml	Hg Densiţy g/cc	Hg Column Height mm	Pressure Dynes/cm ²
CO2-02 Mixtures					
Plenums	20.7	13.5445	13.5441	760.0	1.00831.10 ⁶
C-8	20.3	13.5455	13.5451	758.5	1.00639.106
C-7	20.3	13.5455	13.5451	758.5	1.00639.106
C-10	20.9	13,5440	13.5436	758.3	1.00602.106
C-5	20.4	13.5452	13.5448	757.8	1.00545.106
C-3	20.6	13.5448	13.5444	757.9	1.00555.106
C-9	20.3	13.5455	13.5451	757.9	1.00560.106
C-11	20.8	13.5443	13.5439	758.0	1.00564.10 ⁶

Local acceleration of gravity = 979.558 cm/sec^2

lg/cc = lg/ml * 1.000027

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TABLE -5. Volumetric CO2 Concentrations

. 1

Flask No.	CO2 Volume	CO2 Temp. °C	CO2 Pressure2 Dynes/cm2	CO Density Virial cm /mole	Total Gas Volume cc	Total Gas Temp. °C	Total Gas Pressure Dynes/cm	Total Gas Density Vir. Lcc/mole	Gas Constant erg/°mole	Volumetric CO ₂ Concentrat ppm
CO2-N2	Mixtures									
C-8	1.2978	20.72	1.01070:106	-127.3	5389.1	20.74	1.01079,106	-5.9	8.31436.107	242.04
C-7	1.4619	20.72	1.01070.106	-127.3	5350.2 G	20.74	1.01202,106	-5.9	8.31436.107	274:29
C-10	1.6360	20.72	1.01070.106	-127.3	5329.8	20.73	1.01112.106	-5.9	8.31436.107	308.39
C-5	1.7457	20.72	1.01070,106	-127.3	5320.2	20.73	1.01138.106	-5.9	8.31436.107	329, 58
C-3	1.8359	20.72	1.01070.106	-127.3	5315.0	20.75	1.01121.106	-5.9	8.31436.107	347403
c-9	2.0367	20.72	1.01070.106	-127.3	5237.2	20.76	1.01206.106	-5.9	8.31436.107	390:39
C-11	2.2733	20.72	1.01070.106	-127.3	5224.1	20.74	1.01106.106	-5.9	8.31436.107	437:24
COAr	Mixtures		1076							
	1.2978	20.74	1.01236.10 ⁶	-127.3	5389.1	20.76	1.01367 .10.6	-17:0	8.31436.107	241.63
C-7	1.4619	20.74	1.01236.106	-127.3	5350.2	20.77	1.01243.106	-17.0	8.31436.107	274.51
C-10	1.6360	20.74	1.01236.106	-127.3	5329.8	20.77	1.01383 .106	-17:0	8.31436.107	307.96
C-5	1.7457	20.74	1.01236.106	-127.3	5320.2	20.76	1.01394 .106	-17.0	8.31436.107	329.15
C-3	1.8359	20.74	1.01236.106	-127.3	5315.0	20.76	1.01324 .106	-17:0	8.31436.107	346.73
C-9	2.0367	20.74	1.01236.106	-127.3	5237.2	20.77	1.01366 .106	-17.0	8.31436.107	390.23
C-11	2.2733	20.74	1.01236.106	-127.3	5224.1	20.78	1.01284 .106	-17-0	8.31436.107	437.02
<u>co0</u> 2	Mixtures		1.							
C-8	1.2978	20.75	1.00831 . 10	-127.3	5389.1	20.75	1.00639.10	-17.0	8.31436 .107	242.39
C-7	1.4619	20.75	1.00831 .10	-127.3	5350.2	20.74	1.00639.106	-17.0	8:31436 .107	275.01
C-10	1.6360	20.75	1.00831 .106	-127.3	5329.8	20.76	1.00602.106	-17.0	8.31436 .107	309.08
C-5	1.7457	20.75	1.00831 .106	-127.3	5320.2	20.76	1.00545.106	-17.0	8.31436 .107	330.59
C-3	1.8359	20.75	1.00831 .106	-127.3	5315.0	20.76	1.00555.106	-17.0	8.31436.107	347.98
6-9	2.0367	20.75	1.00831 .106	-127.3	5237.2	20.75	1.00560.106	-17.0	8.31436 .107	391.74
C-11	2.2733	20.75	1.00831.106	-127.3	5224.1	20.76	1.00564.106	-17.0	8.31436.10	438.34

TABLE 6. Index Values, Adjusted Index Values, and Volumetric CO2

Concentrations of Calibrated Gas Mixtures

Flask Number	Plenum Number	Index (Flask Tanks) (ppm)	Adjusted Index (Flask Tanks) (ppm)	Volumetric (ppm)	(Mano	Index pmetric Tanks) (ppm)	Adjusted In (Manometric T. (ppm)	dex anks)
			ำบุ	Mano.	Vd - Equ	<u>a</u> .	74 Mano	Vol-Equ
C-8	P-1	250.14	236.72	42.21 242.04	17	249.50	241.54 235.94	+.50
C-7	. P-2	279.72	272.77	14.17 274.29	+.12	279.40	213.81 272.38	+.48
C-10	P-3	309.01	308.46 3	08.13 308.39	+.26	308.94	308,05 308.38	+.34
C-5	P-4	326.18	329.39	29.2 329.58	+.37	326.23	329,27 329.45	+.31
C-3	P-5	339.94	346.15 3	46.74 347.03	+.29	340.00	346,83 346.23	+.20
C-9	P-6	372.08	385.32 3	90.10 390.39	+.29	372.29	390.40 385.58	01
C-11	P-7	403.46	423.56	35.85 437.24	+1.39	403.82	436.40 424.00	+.84

CO2-N2 Mixtures

N2 !

TABLE	6.	Index	Values.	Adjusted	Index	Values,	and	Volumetric	CO.	

Ar .

Concentrations of Calibrated Gas Mixtures

Flask Number	Plenum Number	Index (ppm)		Adjusted Index (ppm)	Volumetric (ppm)
C-8	P-1	233.05	•	215.90	241.63
·C-7	P-2	260.95		249.90	274.51
C-1 0	P-3	287.86		282.70	307.96
C-5	P-4	303.42		301.65	329.15*
C-3	P-5	316.36		317.42	346.73
C-9	P-6	347.07		354.84	390.23
C-11	P-7	375.62		389.63	437.02

of Calib CO 2-X2 Mixtures stures

* jiggled Hg manometer bulb during equilibration; may have lost some CO₂

TABLE	6.	Index	Values,	Adjusted	Index	Values,	and	Volumetric	<u>co</u> 2
		···· 6:	Indice	a and 1 of	ond the L			tr tions.	2
		Con	centrati	ons of Ca	librate	ed Gas M	ixtu	res	
			ol Cai	st arright	2-12-1	"- vtures			
				CO -N 1	Mixture	es			
				-2(-2					

02!

Flask Number	Plenum Number	Index (ppm)	Adjusted Index (ppm)	Volumetric (ppm)
C-8	P-1	239.87	224.21	242.39
C-7	P-2	268.36	258.93	275.01
C-10	P-3	296.27	292.94	309.08
C-5	P-4	312.54	312.77	330.59
C-3	. P-5	325.77	328.89	347.98
C-9	P-6	356.53	366.37	391.74
C-11	P-7	386.93	403.42	438.34

TABLE 7.. Cubic Coefficients for Volumetric

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vs. 1959 Adjusted Index Plots

Gas	^A 0	<u>A</u>	<u>A2</u>	<u>A</u> 3
N ₂	39.706	0.93795	-8.0035.10-4	1.8923·10 ⁻⁶
Ar	12.580	1.3202	-1.9615.10-43	3.5101.10 ⁻⁶
02	75.027	0.62527	3.6272.10-4	7.9242.10-7

TABLE 8. <u>Comparison of Infrared Analyzer* Response to</u> <u>CO₂-N₂, CO₂-Ar, and CO₂-O₂ Mixtures</u>

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Volumetric	J _{N2}	J _{Ar}	J02	$\frac{J_{N_2} - J_{Ar}}{J_{N_2}}$	$\frac{J_{N_2} - J_{O_2}}{J_{N_2}}$	JN2- JO2 J02
240	234.45	214.34	221.57	0.0858	0.0549	. 058131
260	256.98	234.95	243.26	0.0857	0.0534	,0.56400
- 280	278.80	255.12	264.04	0.0849	0.0559	.055901
300	299.84	274.72	283.99	0.0858	0.0529	.055812
320	320.10	293.66	303.16	0.0826	0.0529	.055918
340	339.56	311.87	321.61	0.0815	0.0529	,055813
360	358.24	329.34	339.39	0.0807	0.0526	055541
380	376.16	346.05	356.55	0.0800	0.0521	.054999
400	393.37	362.04	373.13	0.0796	0.0514	.054244
420	409.88	377.31	389.17	0.0795	0.0505	,053216
440	425.75	391.92	404.70	0.0806	0.0494	,052014
			Ave	r.=0.0824	0.0526	. 055268
				σ =0.0026	0.0018	.001638

*APC Analyzer in 2317 Ritter Hall.

TABLE 9. Carrier Gas Effects on APC Analyzer CO2 Analyses

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20.94690

1959 Adjusted Index (ppm)	Method	Error Caused by 0.93% 0 (ppm)	Error Caused by 0.93% Ar (ppm)	Air Correction† (ppm)
	A Second	Part of Street		
310	Volumetric	3.44	0.24	3.69*
310	Manometric	3.50	0.20**	3.70
320	Volumetric	3.62	0.25	3.88*
320	Manometric	3.68	0.21**	3.89
330	Volumetric	3.81	0.26	4.08*
330	Manometric	3.87	0.23**	4.10

* sum of determined values of 02 and Ar

** difference between values for air and artificial air

+ to be added to CO_2 mole fractions obtained from APC analyzer for air samples measured against CO_2-N_2 standards.

Tank l	Number	Scale Difference Between	Index Difference Between		Scale Difference Between	Index Difference Between		Sample	Flask Average
Primary	High Span	Réference Gases	Reference Gases	Flask No.	Sample and Primary	Sample and Primary	Sample Index	Adjusted Index	Adjusted Index
4297	4288	19.5							
		19.3			H_0-C0.	-N: Mixtures	3		
					Without	dry ice trap	-		
				C-5 C-7 C-8	17.9 37.6 37.4	23.05 48.41 48.15 22.60	340.95 366.31 366.05	347.39 378.29 377.97	347.39 378.29 377.97
				6-3	With d	iry ice trap	341.39	348.17	340.17
				C-3 C-5 C-7 C-8	-0.1 -0.6 19.0 19.0	-0.13 -0.77 24.46 24.46	317.77 317.13 342.36 342.36	319.14 318.36 349.10 349.10	319.14 318.36 349.10 349.10
					N20-CO	-N2 Mixtures	3		
				C-9 C-9	5.7 5.8 7 3	7.34 7.47	325.24 325.37	328.24 328.40 330.75	328.32
4297	4288	19.3 19.2		C-10 C-11	7.4 29.2	9.53 37.59	327.43	330.91 365.10	330.83
Ave	rage of four	19.325	24.88	C-11	29.3	37.72	355.62	365.26	365.18

"TABLE 10. Index Values for CO2-N2-N2O and CO2-N2-H2O Mixtures

Recorder scale factor = 1.28745 ppm/scale division Primary index value = 317.89 ppm

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TABLE 11. N20 Effect on Infrared Analyzer*

Flask No.	Adjusted Index of CO2-N2O-N2	Apparent CO ₂ / (CO ₂ +N ₂ +N ₂ O) Mole Ratio (ppm)	N ₂ 0 Pressure (mm Hg)	Total Pressure (mm Hg)	N ₂ O/ (N ₂ O+N ₂ +CO ₂) Mole Ratio (ppm) (Pressure Ratio)	Adjusted Index of CO ₂ / N ₂ Mixtures	CO2/N2 Mole Ratio (ppm)	Actual CO ₂ / (N ₂ +N ₂ O+CO ₂) Mole Ratio (ppm) Corrected for N ₂ O Dilution	Apparent CO ₂ ppm Seen by Analyzer as Result of N ₂ O	Response Ratio (ppm N ₂ O/ ppm CO ₂
C-9	328,32	328.35	5.1	761.7	6696	318.40	318.29	316.16	12.19	550
C-10	330.82	330.93	9.3	761.8	12208	318.40	318.29	314.40	16.53	740
C-11	365.18	367.65	18.1	761.9	23756	349.90	350.97	342.63	25.02	950

*APC Analyzer in Room 2314 Ritter Hall

TABLE 12. Water Effect on Infrared Analyzer*

lask	Тетр. <u>H₂0 °С</u>	H20 Pressure (mm Hg)	Total Pressure (mm Hg)	H ₂ O/ H ₂ O+CO ₂ +N ₂ Mole Ratio (ppm) (Pressure Ratio)	Adjusted Index Without Dry Ice Trap	Apparent (N ₂ +CO ₂ +H ₂ O) Mole Ratio (ppm)	Adjusted Index With Dry Ice Trap	CO ₂ / (N ₂ +CO ₂) Mole Ratio (ppm)	Actual CO ₂ / (CO ₂ +N ₂ +H ₂ O) Mole Ratio (ppm) Corrected for H ₂ O Dilution	Apparent CO ₂ ppm Seen By Analyzer As Result of H ₂ O	Response Ratio (ppm H ₂ O/ ppm CO ₂)
C-3	22.0	19.827	761.5	26037	348.17	349.12	319.14	319.04	310.73	38.39	680
C-5	21.9	19.709	761.5	25882	347.39	348.29	318.36	318.25	310.01	38.28	680
C-7	22.1	19.951	761.6	26196	378.29	382.43	349.10	350.11	340.94	41.49	630
C-8	22.0	19.827	761.6	26037	377.97	382.06	349.10	350.11	.341.00	41.06	630

*APC Analyzer in Room 2314 Ritter Hall

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TABLE 13. Calibration of Wall Barometer

	Cathetometer (mm)	Readings			Barometer Column		
			Column		Height		
	Atmosphere	Vacuum	Height	Temp. C	(mm)	Temp. C	
	110 0/0						
	110.260				762.1	20.5	
Average	110.261			22.04			
		872.694					
Average		872.696	762.435				
	110.304				762.2	20.5	
Average	$\frac{110.310}{110.307}$		762.389	22.07			
		872.728					
Average		872.740	762 427				
Average	110.360	072.754	102.421		762.2	20.5	
	110.388						
Average	110.374		762.360	22.09			

Average column height = 762.40 mm
temp. = 22.07°CAverage column height = 762.2 mm
temp. = 20.5°Cdensity of Hg = 13.5411 g/mlAverage column height = 762.2 mm
temp. = 20.5°C

Densities obtained from Handbook of Chemistry and Physics 43rd Ed., p. 2157, Chemical Rubber Publishing Co., 1962

To normalize to manometer temperature: Barometer column height = 762.2 mm $\cdot \frac{13.5450}{13.5411} = 762.42$ mm

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VOLUMETRIC REPORT I APPENDIX A

1

J. Alexander Adams Carbon Dioxide Project Scripps Institution of Oceanography La Jolla, California 92093

August 27, 1975

I. Introduction

During January, February, and March 1974, seven five-liter glass flasks, one four-liter manometer flask, and seven glass plenums with volumes from 1 1/4 to 2 1/4 cc had their volumes calibrated. The overall technique in the case of the large flasks was to evacuate the volume to be measured, weigh the flask, fill it with distilled water from which dissolved air had been removed, and weigh again. The difference in the weights, assumed to be the weight of water, was divided by the known density to give the volume. Flasks C-8 and C-11 had this procedure repeated five times; C-3- C-5, C-7, C-9, and C-10 had it done twice. Three runs were made on manometer flask no. 2.

The same technique was used on the plenums, numbered P-1 through P-7, except that mercury was used instead of water. Each was filled and weighed five times.

The large flasks were weighed on a Mettler P-11N single-pan balance, serial no. 474434 in room 0256 Ritter Hall. (This room is part of Professor Harmon Craig's laboratory.) The plenums were weighed on a Seederer-Kohlbusch two-pan 5 kilogram analytical balance, register no. 6971 in 2328 Ritter Hall, using class S rhodium plated brass weights.

Water densities were obtained from the Handbook of Chemistry and Physics, 43rd edition, page 2155, Chemical Rubber Publishing Co., 1962. Mercury densities were from the same source, page 2157.

Values at non-integer temperatures were obtained by linear interpolation between listed densities. The mass per cc was obtained by dividing the mass per ml by 1.000027 (Handbook of Chemistry and Physics, 43rd edition, pages 2157 and 3197).

II. Experimental Procedure

A. Large Glass Flask Calibrations

The procedure for the large flask calibrations was done with with apparatus shown in Figure 1 by the techniques described below.



Figure 1. Apparatus to Fill Large Glass Flasks with Water

Stopcock "C" is a 120° glass stopcock with the following positions:



Stopcock "A" is an oblique bore glass vacuum stopcock to let air into the system; stopcock "B" is a hollow plug glass vacuum stopcock attached to the flask; stopcock "D" is a standard straight bore separatory funnel glass stopcock; stopcock "E" is a "T" three-way glass vacuum stopcock.

The apparatus was assembled with the stopcocks greased with Apiezon "N" lubricant. Liquid nitrogen was placed on both of two cold traps adjacent to the vacuum pump (not shown in Figure 1). Just enough liquid nitrogen was placed around the water trap to touch its bottom. A higher level of refrigerant was avoided to reduce tendency of the trap to plug up with ice.

Initially the flask to be calibrated was evacuated on another vacuum line and installed in the filling apparatus. With the filling system at ambient pressure stopcock "A" was closed and stopcock "E" was slowly opened to evacuate the system. Stopcock "C" was set in position 1. After evacuation was completed, the separatory funnel was filled with de-ionized water from the tap in 2328 Ritter Hall and the magnetic stirrer started. Stopcock "D" was opened slightly and water admitted to the 4000 ml boiling flask. The separatory funnel was filled with additional water if necessary to complete the filling of the boiling flask.

When the boiling flask was filled to near the top, stopcock "D" was closed and the water boiled for five to ten minutes under vacuum. If the top of the water trap got too cold, the water coming into the trap froze in the end of the inlet tube from the boiling flask and plugged it. To unplug it, stopcock "E" was closed, stopcock "A" was slowly opened to the air, and the water trap heated with a heat gun until the ice plug fell off. Then stopcock "A" was closed, stopcock "E" slowly opened, and the operation continued.

After five to ten minutes had elapsed without interference of any plug of ice, stopcock "C" was turned to position 2 for about thirty seconds to evacuate the siphoning tube, and the magentic stirrer was turned off. Stopcock "C" was then turned to position 3.

Stopcock "E" was closed and stopcock "A" was slowly opened to air. The water was thus forced up the siphoning tube and filled the tube running from the 4000 ml boiling flask to the flask to be calibrated.

Stopcock "B" was opened slightly and water admitted to the flask to be calibrated until the water level in the 4000 ml boiling flask was close to the bottom of the siphoning tube. Then stopcock "B" was closed. To prepare additional degassed water, stopcock "A" was closed and stopcock "E" slowly opened. After about one minute of evacuation, stopcock "C" was turned to position 1. The magnetic stirrer was turned on and stopcock "D" was opened slightly to refill the 4000 ml boiling flask. Then stopcock "D" was closed and the water boiled under vacuum for five to ten minutes. The magnetic stirrer was then turned off and the previous procedure used to complete filling of the flask to be calibrated.

After filling, the water in the flask to be calibrated was slightly heated with a heat gun with the system still open to the vacuum pump via stopcock "E". Bubbles were jarred loose from the bottom half of the flask by tapping. The water was warmed to about 2° above ambient temperature and boiled for ten minutes under vacuum. Then stopcock "E" was closed, stopcock "A" slowly opened to let air pressure into the system and force water into the flask.

After boiling, an air bubble at 1 atm pressure and about 10 cc volume always remained in stopcock "B". To remove it the following procedure was used:

Stopcock "A" was closed and stopcock "E" was slowly opened to pull the bubble out through the vacuum pump. Stopcock "B" was closed and stopcock "C" turned to position 2 for about thirty seconds, then to position 3 to remove any air still in the system. Stopcock "E" was closed, stopcock "A" slowly opened and stopcock "B" opened slightly to admit water into the volume formerly occupied by the air bubble. Stopcock "B" was opened fully when water had ceased to flow. If any small residual bubble remained in the stopcock "B", then stopcock "A" was closed, stopcock "E" slowly opened, and after about thirty seconds the procedure was repeated.

Up to a dozen 1 mm diameter bubbles at atmospheric pressure were allowed to remain, as they would later be absorbed into the water, which was greatly undersaturated with respect to dissolved air at 1 atmosphere pressure.

The flask to be calibrated was carefully removed from the line, leaving stopcock "B" open. A glass tube with a 14/35 female ground glass fitting on one end was placed over a corresponding male fitting above stopcock "B" and filled with distilled water. Then the flask stood overnight to reach temperature equilibrium and allow absorption of air bubbles in the water.

Before weighing, stopcock "B" was closed, the tube removed from the flask neck above stopcock "B", and the water removed from the inside of the flask neck. Grease and water were cleaned from the flasks exterior with trichloroethylene and the ambient temperature was recorded. The flask was then weighed.

The small amount of dissolved air still in the water probably could not affect the calibration results significantly because water saturated with air at 1 atmosphere pressure has a density lower than that of pure water by about 3 parts in 10⁶ (International Critical Tables, Vol. 3, Page 26). Since the water in the flask was greatly undersaturated, any error in density owing to dissolved air was negligible.

B. Calibration of Plenums

The design of a plenum is shown in Figure 2.



Figure 2. CO₂ Plenum

With the plenum chamber previously evacuated, mercury was injected into the hollow plug of the stopcock with a syringe attached

to a teflon spaghetti tube which was small enough to pass through the neck above the stopcock into the plug. The bore of the hollow plug was about 2/3 filled with mercury, and the stopcock was turned so that the bore hole was below the surface of the murcury, but not open to the plenum chamber. The air was removed from the space in the stopcock above the mercury in order to dislodge and remove any air bubbles trapped in the bore under the mercury. Air pressure was restored over the mercury, and the stopcock was opened slightly to admit the mercury into the plenum chamber slowly. When the plenum had been filled, the stopcock was opened fully to the chamber and again the air was evacuated from above the mercury to remove any further trapped air bubbles. After thirty minutes of temperature equilibration, the stopcock was closed and excess mercury poured out of the stopcock plug bore. Ambient temperature was recorded. The inside of the stopcock was then rinsed with nitric acid followed by distilled water and the plenum attached to a vacuum line and evacuated to dry out the water still remaining inside the stopcock. The plenum was removed and its exterior cleaned with trichloroethylene. The plenum was then weighed. The air bubble problem was less serious than in the case of the large flasks, since air does not dissolve appreciably in mercury.

C. Preparation for Recalibration

The water was removed from the large flasks by removing the stopcock plugs and draining. The stopcocks were then cleaned of

grease and regreased. The flasks were evacuated to dry out all residual water. To remove mercury from the plenums, the stopcocks were opened, the plenums turned nearly upside down so that the mercury fell into the end of the stopcock plug near the handle, and the air removed from the stopcock plug. The mercury fell from the plenum chamber into the stopcock plug, whence it was poured out. The stopcock plug was removed, all surfaces cleaned of grease, and a teflon spaghetti tube pushed in so that its end was at the closed end of the plenum chamber. Through this tube the plenums were rinsed with nitric acid followed by water, all injected by a syringe attached to the tube. The aqueous liquids were shaken out of the plenum chambers. The plenum stopcocks were then air-dried and regreased. The plenum chambers were evacuated to dry.

III. Calculations and Results

Nine weighings were made on each evacuated flask and nine more on each after filling with water, except that in the first filling of flask C-8, six weighings each were made on the evacuated and full flask. Each plenum was weighed three times evacuated and three times filled with mercury. Mean weights and volumes were then computed. The standard deviation for the weights of water or mercury was computed as the square root of sum of squares of standard deviations of weights empty and full.

A universal standard deviation for a single plenum weighing or large flask weighing was calculated by the formula 1 stt

$$\sigma_{\text{universal}} = \left(\frac{\sum_{i=1}^{N} \sum_{i=1}^{M} (X_{ij} - \overline{X}_{i})^2}{\sum_{i=1}^{N} M_{i} - N} \right)^{1/2}$$

where X_{ij} was the jth weight measurement for the ith full or empty vessel; \overline{X}_i was the average weight for the ith vessel; M_i was the number of weighings made on the ith vessel; and N was the number of vessels. The σ for weight of water or mercury was $\sigma_{universal} \cdot \sqrt{2}$, since these weights were differences between two measured weights. The $\sigma_{universal}$ for volumes due to weighing uncertainty was $\sigma_{universal}$ for weights divided by liquid densities -- 1.0g/cc for water and 13.54g/cc for mercury.

Tables 1 and 2 list the results of the flask calibrations;Table 1Table 3 and 4 list the results of the plenum calibrations.Table 5Table 3 and 4 list the results of the plenum calibrations.Table 5Ists the standard deviations, and standard deviations of the means.Table 1

The $\sigma_{universal}$ for volume measurements from individual fillings of flasks and plenums was calculated by the above formula, where X_{ij} was the jth volume measurement of the ith vessel; X_i was the average volume for the vessel; M_i was the number of volume measurements made on the ith vessel; and N was the number of vessels. This was assumed to be $\sigma_{universal}$ (total) for the volumes.

This $\sigma_{universal}$ for volume measurements was partitioned into uncertainty due to weighing and uncertainty due to filling changes. If it was assumed that $\sigma_{universal}^2$ (weighings) + $\sigma_{universal}^2$ (fillings) = $\sigma_{universal}^2$ (total), and $\sigma_{universal}$ (weighings) and $\sigma_{universal}$ (total) were already available then $\sigma_{universal}$ (fillings) could be calculated. Standard deviations of the mean values were the $\sigma_{universal}$'s divided by the square root of number of measurements made for each mean. Relative uncertainty was absolute uncertainty divided by the value of the measurement (a "standard" volume for flasks and plenums is indicated in Table 5).

In June of 1976 the Mettler PllN single-pan balance used in the above experiment was calibrated using Class S rhodium-plated brass weights. Two 1-kg weights and one 2-kg weight were used. In addition a glass bottle of mercury, weighed on the Seederer-Kohlbusch two-pan balance at 2826.8 g, was used. These weights were weighed on the P11N. The readings obtained from the P11N Table 6 are listed in Table 6. Weighings were done for 1 kg, 2 kg, 2.8268 kg, and 6.8268 kg. In general, it can be noted that "true" readings were obtained if the weights were quickly placed on the pan. If they were held so they gradually settled on the pan (over a period of 2-3 seconds) the scale reading was from 1/2 to 2 grams low. The difference seemed to be independent of weight on the pan. Sometimes tapping the side of the balance caused the pan to settle further so that a truer reading was obtained. However, this did not cause concern as far as the volume calibrations were concerned for two reasons: (1) The volumes were based on differences between full and empty weights. Errors caused by "settling" the weights onto the pan would tend to cancel out. (2) o for the volume was 0.64 cc,

so this error could arguably be called statistical, since 30 is about 2 cc.

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Apparently, however, the balance tends to bind at an erroneously low weight reading if the pan is pushed down too slowly by the weights.

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	Flask	No. C-8,	Filling No. 1		Flask No. C-8, Filling No. 2					
	Evacuated	Flask	Full Flask			Evacuated		Full Flas	k	
•						Wt. No.	Wt.(g)		Wt. No.	Wt.(g)
B Jan	74 Wt. No.	Wt.(g)	9 Jan 74 Wt. No.	Wt.(g)	9 Jan 74	1	780.5	10 Jan	74 1	6161.9
	1	782.4	i	6162.4		2	780.6	1.	2	6161.9
	2	782.1	2	6162.4		3	779.3		3	6161.2
	3	782.0	3	6162.2		4	780.6		4	6162.1
	4	782.2	. 4	6162.3		5	780.6		5	6162.0
	5	782.3	. 5	6162.6		6	781.0		6	6162.1
	6	782.1	6	6162.3		7	781.0		7	6162.7
	Average	= 782.2	Average =	6162.4		8	780.3		8	6161.8
		,				9	779.8		9	6162.1
		Wt.	Water = 5380.2 g			Average	= 780.4		Average	= 6162.0

UYR

Wt. Water = 5381.6 g

0

Flask No. C-8, Filling No. 3 Flask No. C-8, Filling No. 4 Evacuated Flask Evacuated Flask Full Flask Full Flask 10 Jan 74 Wt. No. Wt.(g) 11 Jan 74 Wt. No. Wt.(g) 11 Jan 74 Wt. No. Wt.(g) 14 Jan 74 Wt. No. Wt.(g) 779.2 1 6163.6 1 779.6 1 6162.0 1 2 780.5 6162.7 2 780.1 2 6162.1 2 781.4 6162.6 780.5 6162.7 3 3 3 3 6162.4 780.7 6162.3 4 779.8 4 4 4 780.4 6162.6 5 780.0 5 6162.0 5 5 6 780.5 6 6162.6 778.9 6 6162.2 6 780.5 6162.1 780.5 6162.0 7 7 7 7 6162.7 780.5 6162.0 780.8 8 8 8 8 780.9 9 6162.5 780.9 9 6162.8 9 9 Average = 6162.3Average = 780.4Average = 6162.6Average = 780.2= 0 5 3 = 0.7

0 = G.

Wt. Water = 5382.2 g

+ - 11 G 11

Wt. Water = 5382.1 g

- 0 S g

2.

	Flask	No. C-8, 1	Filling No. 5		Flask No. C-11, Filling No. 1						
	Evacuated	Flask	Full Flask			Evacuated	Flask	F	ull Flask		
14 Jan	n 74 Wt. No.	Wt.(g)	15 Jan 74 Wt. No.	Wt.(g)	17 Jan 74	Wt. No.	Wt.(g)	18 Jan 74	WtNo.	Wt.(g)	
	1	780.1	1	6160.5		1	991.6		1	6206.3	
	2	781.5	2	6161.1		2	991.4		2	6207.0	
	3	780.8	3	6160.5		3	991.4		3	6206.3	
	4	780.8	4	6160.2		4	991.8		4	6206.5	
	5	779.6	5	6160.7		5	991.0		5	6206.3	
	6	781.3	. 6	6161.0		6	990.4		6	6206.	
	7	780.2	7	6160.4		7	991.6		7	6206.0	
	8	781.4	8	6160.4		8	991.3		8	6206.	
	9	781.9	9	6160.8		9	991.4		9	6207.0	
	Average	= 780.8	Average =	6160.6		Average	= 991.3	See State	Average =	6206.0	
		- 1.8		0.1						6.3	

Wt. Water = 5379.8 g

0 = () 9 g

Wt. Water = 5215.3 g

~ - 0.5 g

Flask No. C-11, Filling No. 2

Flask No. C-11, Filling No. 3

	Evacuated	i Flask	Full Flask			Evacuated	Flask	Full Flask	
18	Jan 74 Wt. No.	Wt.(g)	21 Jan 74 Wt. No.	Wt.(g)	21 Jan 74	Wt. No.	Wt.(g)	22 Jan 74 Wt. No.	Wt.(g)
	1	992.2	1	6207.5		1	991.6	1	6208.4
	2	991.1	2	6208.5		2	992.1	2	6209.4
	3	991.3	3	6208.3		3	991.9	3	6208.6
	4	991.8	4	6208.3		4	991.7	4	6207.2
	5	990.8	5	6208.8		5	992.3	5	6209.5
	6	991.5	. 6	6209.1		6	992.6	6	6209.5
	7	991.6	7	6209.0		7	992.1	. 7	6207.7
	8	991.3	8	6209.0		8	991.9	. 8	6209.8
	9	991.1	9	6209.3		9	991.3	. 9	6209.1
	Average	e = 991.4	Average =	6208.6		Average	= 991.9	Average =	6208.8

Wt. Water = 5217.2 g

a = 0.8 g

Wt. Water = 5216.9 g

c = 1 5 g

- = 1. 1

Flask No. C-11, Filling No. 4							Flask No. C-11, Filling No. 5							
		Evacuated	Flask	Fu	ill Flask		·		Evacuated	Flask		Fu	ll Flask	
22 J	an 7	4 Wt. No.	Wt.(g)	23 Jan 74	Wt. No.	Wt.(g)		23 Jan 74	Wt. No.	Wt.(g)	24 Ja	n 74	Wt. No.	Wt.(g)
		1	991.1		1	6205.7			1	990.7			1	6205.0
		2	991.5		2	6205,9			2	991.2			2	6204.6
		3	991.6		3	6205.8			3	991.9			3	6205.0
		4	991.3		4	6205.3			* 4	991.5			4	6204.6
		5	991.8		5	6205.3			5	991.3			5	6204.2
		6	992.2		6	6205.3			6	991.7			6	6204.9
		7	991.1		7	6205.3			7	990.6			7	6205.2
		8	992.7		8	6205.4			8	991.4	• •		8	6205.2
		9	991.8		9	6205.3			9	991.8			9	6204.7
		Average	= 991.7	I	verage =	6205.5			Average	= 991.3		A	verage =	6204.8
							·							

. = [1 n

.

Wt. Water = 5213.8 g

. 0. g

Wt. Water = 5213.5 g

e 6 5

	Flask	No. C-11,	Filling N	0.6		Flask No. C-3, Filling No. 1						
	Evacuated	Flask		Full Flask			Evacuated	Flask	Fu	111 Flask		
24 Jan	74 Wt. No.	Wt.(g)	25 Jan	74 Wt., No.	Wt.(g)	28 Jan 74	Wt. No.	Wt.(g)	29 Jan 74	Wt. No.	Wt.(g	
	1	991.2		1	6205.8		1	905.9		1	6211.	
	2	992.0		2	6205.9		2	907.2		2	6211.	
	3	992.1		3	6205.8		3	906.8		3	6210.	
	4	992.1		4	6205.8		4	906.6		4	6210.	
	5	992.4		5	6206.1		5	907.1		5	6211.	
	6	992.2		• 6	6205.9		6	906.0		6	6210.	
	7	991.7		7	6205.7		7	907.0		7	6211.	
	8	991.9		8	6205.7		8	906.4		8	6211.	
	9	991.6		9	6206.0		9	906.4		9	6210.	
	Average	= 991.9		Average =	6205.9		Average	= 906.6		Average =	6211.	

a = 0.4

Wt. Water = 5214.0 g

Wt. Water = 5304.5 g

= 0.6 g

0
rtask No. C-J, ritting No. 2	F.	lask	No.	C-3,	Filling	No.	2
------------------------------	----	------	-----	------	---------	-----	---

Flask No. C-5, Filling No. 1

	Evacuated Flask			Full Flask		'		Evacuated	Flask		Fu	ll Flask	
29	Jan 74 Wt	. No.	Wt.(g)	30 Jan 74 Wt. No.	Wt.(g)	28	Jan 74	Wt. No.	Wt.(g)	29	Jan 74	Wt. No.	Wt.(g)
		1	907.2	1	6211.3			1	882.1			1	6190.5
		2	907.7	2	6211.1			2	880.4			2	6190.8
		3	906.8	3	6210.9			3	881.3			3	6190.7
		4	907.2	. 4	6211.6			4	881.5			4	6190.3
		5	906.2	5	6210.7			5	880.7			5	6190.8
		6	907.5	. 6	6211.0		•	6	881.2			6	6191.3
		7	907.3	7	6210.5			7	881.1			7	6191.1
		8	907.0	8	6211.3			8	880.5			8	6191.1
		9	908.3	9	6211.3			9	881.3			9	6190.9
	Av	erage	= 907.2	Average =	6211.1			Average	= 881.1			Average =	6190.8
			6		6.4			3	= 0.6			. E	

Wt. Water = 5303.9 g

Wt. Water = 5309.7 g

0.7 2

- 0.8 g

Flask No. C-5, Filling No. 2

TABLE 1. Flask Weights

Flask No. C-7, Filling No. 1

Evacuated Flask Full Flask Evacuated Flask Full Flask 29 Jan 74 Wt. No. Wt.(g) 30 Jan 74 Wt. No. Wt.(g) 28 Jan 74 Wt. No. Wt.(g) 29 Jan 74 Wt. No. Wt.(g) 1 881.8 6190.3 6236.7 1 1 897.7 1 881.4 6190.6 2 2 2 897.3 2 6236.8 881.3 3 3 6190.3 3 898.4 3 6236.9 4 881.7 . 4 6190.9 4 897.9 6236.9 4 880.8 6190.6 6236.9 898.2 5 5 5 5 6 881.3 6 6190.9 6 897.8 6 6236.6 7 881.9 6190.2 7 7 6236.4 7 897.0 8 882.0 8 6190.0 8 897.6 8 6236.8 9 881.7 9 6190.9 9 897.2 9 6237,1 Average = 6190.5Average = 897.7 . Average = 6236.8 Average = 881.5- - - 3 3

Wt. Water = 5309.0 g

Wt. Water = 5339.1 g

Û. 0

 $\sigma = 0.5$

J = C ig

Flask No. C-7, Filling No. 2

Flask No. C-9, Filling No. 1

	Evacuated Flask		Full Flask		1	Evacuated	Flask		Fu	11 Flask	
29	Jan 74 Wt. No.	Wt.(g)	30 Jan 74 Wt. No.	Wt.(g)	30 Jan 74	Wt. No.	Wt.(g)	31	Jan 74	Wt. No.	Wt.(g)
	1	896.9	1	6236.9		1	999.9			1	6227.5
	2	897.8	2	6236.7		2	1000.4			2	6227.5
	3	897.5	3	6236.3		3	999.8			3	6227.3
	4	897.8	4	6237.0		4	1000.0			4	6227.5
	5	897.2	5	6237.3		5	1001.7			5	6227.6
	6	897.3	• 6	6237.1		6	999.9			6	6227.9
	7	897.7	7	6237.0		7	1000.2			7	6227.3
	8	897.5	8	6236.8		8	1000.9	,		8	6227.1
	9	896.9	9	6237.3		9	1000.7			9	6227.4
	Average	897.4	Average =	6236.9		Average =	1000.4		A	verage =	6227.5
			S	1							

Wt. Water = 5339.5 g

. - 0.5 g

Wt. Water = 5227.1 g

0 = 0.8 8

Flask No. C-9, Filling No. 2

Flask No. C-10, Filling No. 1

	Evacuated Flask				Full Flask		,			Evacuated	Flask			Full Flask	
31 J	an 74	Wt. No.	Wt.(g)	1 Feb	74 Wt. No.	Wt.(g)		30 Jan	74	Wt. No.	Wt.(g)	3	31 Jan 7	4 Wt. No.	Wt.(g)
		1	1000.6		í	6226.9				1	900.0			1	6218.8
		2	1001.3		2	6227.3				2	900.5			. 5	6218.9
		3	999.8		3	6226.7				3	900.3			3	6219.1
		4	1001.9		4	6227.1				4	901.0			4	6219.2
		5	1000.6		5	6226.4				5	899.7			5	6219.4
		6	1000.5		6	6227.1				6	899.5			6	6219.2
		7	1002.0		. 7	6227.2				7	900.2			7	6218.9
		8	1000.1	*	8	6227.1				8	899.5			8	6219.3
		9	1000.2		9	6226.0				9	900.5			9	6219.1
		Average	= 1000.8		Average =	6226.9		•		Average	= 900.1			Average =	6219.1

- - 0.8

Wt. Water = 5226.1 g

Wt. Water = 5319.0 g

= 1.5

0 * * 6

- 1 - 5

	Flask	No. C-10,	Filling No. 2			Manometer	Flask No	. 2, Filling	<u>No. 1</u>	
	Evacuated	Flask	Full Fla	ask		Evacuated	Flask	Fu	11 Flask	
31 Jan	74 Wt. No.	Wt.(g)	1 Feb 74 Wt. 1	No. Wt.(g)	28 Mar 74	Wt. No.	Wt.(g)	29 Mar 74	Wt. No.	Wt.(g)
	1	900.1	1	6218.9		1	1120.3		1	5057.7
	2	900.0	2	6219.1		2	1121.7		2	5059.3
	3	899.4	3	6219.0		3	1121.0		3	5059.0
	4	900.2	4	6219.3		4	1121.3		4	5058.9
	5	900.4	5	6218.1		5	1121.3		5	5059.0
	6	900.8	• 6	6219.2		6	1121.5		6	5058.6
	7	900.0	7	6219.4		7	1121.1		7	5058.8
	8	899.3	. 8	6219.5		8	1121.4		8	5059.5
	9	900.2	9	6219.3		9	1121.4		9	5059.0
	Average	= 900.0	Averag	e = 6219.1		Average =	1121.2		Average =	5058.9

0 = 0.5

Wt. Water = 5319.1 g

Wt. Water = 3937.7 g

5 0.7

0

		Manometer	Flask No. 2	2, Filling No.	. 2		••		Manome	eter 1	Flask No.	2, F1	ling N	0.3	
		Evacuated	Flask	Ful	1 Flask		2		Evacua	ated 1	Flask		Ful	1 Flask	
29	Mar 7	4 Wt. No.	Wt.(g)	1 Apr 74	Wt, No.	Wt.(g)		1 Apr 74	Wt. 1	No.	Wt.(g)	2 /	pr 74	Wt. No.	Wt.(g)
		1	1121.0		1	5059.5			1		1121.0			1	5058.3
		2	1119.9		2	5059.2			2		1121.2			2	5059.4
		3	1121.2		3	5059.3			3		1120.9			3	5059.5
		4	1120.8		4	5058,9			4		1120.8			4	5059.3
		5	1120.8		5	5059.2			5		1120.7			5	5059.2
		6	1121.0		6	5058.9			6		1120.8			6	5059.3
		7	1121.1		7	5059.0			7		1119.9			7	5059.6
		8	1121.0		8	5059.5			8		1121.3			8	5059.8
		• 9	1120.6		9	5058.7			9		1120.9			9	5059.5
		Average •	= 1120,8	Av	verage =	5059.1			Avera	ge =	1120.8		A	verage =	5059.3
			•												

Wt. Water = 3938.3 g

4 = 0.5 E

03

Wt. Water = 3938.5 g

a = 0.1g

TABLE 2. Flask Volumes

	Date		Book No.	Page No.	Wt. of Water (g)	σ(g) ^{†Wa}	ater temp. (°C)	Density of Water (g/cc)	Computed Flask Volume (cc)
		•			Flask No	b. C-3.	ġ.c.		
29	Jan	74	1	134	5304.5	0.64	21.0	0.997992	5315.2
30	Jan	74	1	135	5303.9	0.64	21.2	0.997948	5314.8
								Average volume	= 5315.0 cc
					Flask No	<u>o. C-5</u>			
29	Jan	74	1	136	5309.7	0.64	21.0	0.997992	5320.4
30	Jan	74	1	137	5309.0	0.64	21.2	0.997948	5319.9
								Average volume	= 5320.2 cc
					Flask N	<u>o. C-7</u>			
29	J.an	74	1	138	5339.1	0.64	21.0	0.997992	5349.8
30	Jan	74	1	139	5339.5	0.64	21.2	0.997948	5350.5
								Average volume	= 5350.2 cc

to universal for Mettler P-11 balance given.

TABLE 2. Flask Volumes

			Book	Page	Wt. of	W	ater temp.	Density; of Water	Computed Flask Volume
	Date	2	No.	No.	Water (g)	<u>σ(g)</u> [†]	(°C)	(g/cc)	<u>(cc)</u>
					Flask N	lo. C-8	-		
9	Jan	74	1	121	5380.2	0.64	18.5	0.998501	5388.3
10	Jan	74	1	122	5381.6	0.64	18.8	0.998444	5390.0
11	Jan	74	1	123	5382.2	0.64	17.3	0.998722	5389.1
14	Jan	74	1	124	5382.1	0.64	18.1	0.998576	5389.8
15	Jan	74	1	125	5379.8	0.64	19.1	0.998385	5388.5
								Average volume	= 5389.1 cc
					Flask N	No. C-1			
17	Jan	74	1	127	5215.3	0.64	21.0	0.997992	5225.8
18	Jan	74	1	128	5217.2	0.64	17.9	0.998613	5224.4
22	Jan	74	1	129	5216.9	0.64	16.3	0.998893	5222.7
23	Jan	74	1	130	5213.8	0.64	20.3	0.998141	5223.5
24	Jan	74	1	131	5213.5	0.64	21.2	0.997948	5224.2
25	Jan	74	1	132	5214.0	0.64	20.5	0.998099	5223.9

Average volume = 5224.1 cc

* Handbook of Chemistry and Physics, 43rd Edition, page 2155, Chemical Rubber Publishing Co., 1962.
† σ_{universal} for Mettler P-11 balance given.

						-			
	Date		Book No.	Page No.	TABLE 2. H Wt. of Water (g)	$\frac{\sigma(g)}{\sigma(g)}^{+W}$	olumes ater temp. (°C)	Density of Water (g/cc)	Computed Flask Volume (cc);
				,	Flask	No. C-	9		
31	Jan	74	1	140	5227.1	0.64	21.1	0.997970	5237.7
1	Feb	74	14	141	5226.1	0.64	21.0	0.997992	5236.6
								Average volume =	= 5237.2 cc ²
					Flask	No. C-	10		
31	Jan	74	1	142	5319.0	0.64	21.1	0.997970	5329.8
1	Feb	74	1	143	5319.1	0.64	21.0	0.997992	5329.8
								Average volume =	= 5329.8 cc
					Manomete	er Flas	ik #2		
29	Mar	74	2	31	3937.7	0.64	22.1	0.997747	3946.6
1	Apr	74	2	32	3938.3	0.64	21.9	0.997792	3947.0
2	Apr	74	2	33	3938.5	0.64	21.8	0.997815	3947.1
								Average volume	= 3946.9 cc
Jun	iver	sal o	f balan	ce (based on	426 weighin	lgs, 48	averages)	= 0.45 g.	
Jour	iver	sal o	f weight	ts of water	(differences	betwe	en empty an	nd full flasks) = g($0.45\sqrt{2} g = 0.64 g.$
σur	iver	sal ^o	f volume	e due to weig	ghings = 0.6	64 cc			
σun	iver	sal ^o	f indiv:	idual volume	determinati	lons =	(based on 2	24 fillings, 8 aver	ages) = 0.74 cc
σur	iver	sal o	of volum	e due to rep	etitive fill	lings w	ith water =	= 0.37 cc	

† σuniversal for Mettler P-11 balance given.

Plenum No. P-1

	1	Evacuate	d Plenu	m	Full Plen	um	1	Evacuated	l Plenum	Fu	11 Plenu	m
		Wt. No.	Wt.(g)		Wt. No	. Wt.(g)		Wt. No.	Wt.(g)		Wt. No.	Wt.(g)
				Filling No. 1					Fi	lling No. 4		
28 Feb	74	1	52.407	1 Mar	74 1	69.984	11 Mar 74	1	52.419	11 Mar 74	1	69.998
		2	52.408		2	69.983		2	52.418	2	2	69.998
		3	52.406		3	69.983		3	52.418		3	69.999
11	A	verage =	52.407	1 190 R	Average	= 69.983	10 m m m m m m m m m m m m m m m m m m m	Average =	52.418	1	verage =	69.998
			Wt.	Mercury = 17.57	3 g*				Wt. Me	rcury = 17.577	' g*	
				Filling No. 2	•				Fi	lling No. 5		
4 Mar	74	1	52.408	5 Mar	74 1	69.985	13 Mar 74	1	52.415	13 Mar 74	1	69.996
		2	52.409		2	69.985		2	52.415	4	2	69.994
		3	52.409		3	69.985		3	52.416		3	69.996
	A	verage =	= 52.409		Average	= 69,985		Average •	= 52.415	1	verage =	69.995
		15.14	Wt.	Mercury = 17.57	13 g*				Wt. Me	ercury = 17.57	/ g*	
				Filling No. 3								
6 Mar	74	1	52.401	8 Mar	74 1	69.980						
		2	52.400		2	69.981						
		3	52.400		3	69.980						
	A	verage =	= 52.400		Average	= 69.980						
			Wt.	Mercury = 17.57	17 g*							

* Buoyancy correction for weights = -0.003 g added to weight of mercury.

TABLE 3. Plenum Weights Plenum No. P-2

		Evacuate	d Plenu	n	Fu	11 Plenum	ı .		Evacuated	Plenum	Fu	11 Plenu	n
		Wt. No.	Wt.(g)			Wt. No.	Wt.(g)		Wt. No.	Wt.(g)		Wt. No.	Wt.(g)
				Filling No. 1	L				•	1	Filling No. 4		
28 Feb	74	1	52.442	28 Fel	5 74	1	72.244	. 11 Mar 74	1	52.439	12 Mar 74	1	72.243
		2	52.442	1 May	-	2	72.244		2	52.438		2	72.242
		3	52.442			3	72.244		3	52.439		3	72.242
	A	verage =	52.442			Average =	72.244		Average =	52.439	A	verage =	72.242
			Wt. 1	Mercury = 19.2	799	g*				Wt. 1	Mercury = 19.800) g*	
				Filling No.2	•						Filling No. 5		
4 Mar	74	1	52.443	4 Mai	. 74	1	72.242	13 Mar 74	1	52.442	14 Mar 74	1	72.239
		2	52.444	2		2	72.243		2	52.442		2	72.239
		3	52.443			3	72.241		3	52.441		3	72.238
	A	verage =	52.443			Average =	72.242		Average =	52.442	A	verage =	72.239
			Wt. 1	Mercury = 19.	796	g*				Wt.	Mercury = 19.794	f g*	
				Filling No.	3								
7 Mar	74	1	52.439	8 Mar	c 74	1	72.240						
		2	52.438			2	72.240						
		3	52.438			3	72.240						
	A	verage =	52.438			Average =	72.240						
			Wt. 1	Mercury = 19.3	799	g*							

*Buoyancy correction for weights = -0.003 g added to weight of mercury

Plenum No. P-3

	I	Evacuate	d Plenu	m	Full Plenu	Im		Evacuated	Plenum	Ft	ull Plenu	n
		Wt. No.	Wt.(g)	Filling No. 1	Wt. No.	Wt.(g)		Wt. No.	Wt.(g)	Hiling No. 4	Wt. No.	Wt.(g)
29 Pob	71.	1	54 000	1 Mar	7/ 1	76 949	11 Mar 74		E4 090	12 Non 7/		76 247
zo red	0 74	T	54.090	1 Mar	74 1	76.248	11 Mar /4	1	54.089	12 Mar 74	1	10.241
		2	54.090		2	76.248		2	54.089		2	76.247
		3	54.090		3	76.248		3	54.089		3	76.246
	A	verage =	54.090		Average	= 76.248		Average =	54.089	1	Average =	76.247
			Wt.	Mercury = 22.15	5 g*				Wt. M	lercury = 22.15	5 g*	
				Filling No. 2	•				F	illing No. 5		
4 Mar	74	1	54.088	Mar	74 1	76.249	13 Mar 74	1	54.092	14 Mar 74	1	76.247
		2	54.090	5	2	76.246		2	54.091		2	76.248
		3	54.090		3	76.249		3	54.091		3	76.247
					4	76.248						
	A	verage =	54.089		Average	= 76.248		Average =	54.091		Average =	76.247
			Wt.	Mercury = 22.15	6 g*				Wt. M	fercury = 22.15	3 g*	
				Filling No. 3								
7 Mar	74	1	54.087	8 Mar	74 1	76.245						
		2	54.087	÷ .	2	76.245						
		3	54.087		3	76.245						
	A	verage =	54.087		Average	= 76.245						
			Wt.	Mercury = 22.15	5 g*							

* Buoyancy correction for weights = -0.003 g added to weight of mercury.

Plenum No. P-4

	Evacuated Plenum			Full Plenum				
		Wt. No	. Wt.(g)		Wt.	No.	Wt.(g)	
			Fil	ling No. 1				
25 Fe	ъ 74	1	57.529	26 Feb	74 1		81.179	7
		2	57.530		2		81.180	
		3	57.530		3		81.178	
	Av	erage	= 57,530		Aver	age =	81.179	
			Wt. Merc	ury = 23.64	46 g*			
			<u>F11</u>	ling No. 2	•			
1 Ma	r 74	1	57.526	1 Mar	74 1		81.168	11
		2	57.525		2		81.168	
		3	57.525		3		81.168	
	Av	erage	= 57.525		Aver	age =	81.168	
			Wt. Merc	ury = 23.64	40 g*			
			Fil	ling No. 3				
4 Ma	r 74	1	57.521	5 Mar	74 1		81.162	
		2	57.521		2		81.160	
		3	57.521		3		81.161	
	Av	erage	= 57.521		Aver	age =	81.161	
			Wt. Merc	ury = 23.6	37 g*			

			Wt. No.	Wt.(g)		Wt. No.	Wt.(g)
				Fi	lling No. 4		
7	Mar	74	1	57.521	8 Mar 74	1	81.167
			2	57.521		2	81.169
			3	57.520		3	81.167
			Average =	57.521	A	verage =	81.168
				Wt. Me	rcury = 23.644	g*	· · ·
				Fi	lling No. 5		
.1	Mar	74	1	57.519	12 Mar 74	1.4	81.169
			2	57.519		2	81.167
			3	57.520		3	81.167
	•		Average =	57.519	A	verage =	81.168
				Wt. Me	rcury = 23.646	8*	-

Evacuated Plenum

Full Plenum

* Buoyancy correction for weights = -0.003 g added to weight of mercury.

Plenum No. P-5

	E	vacuate	d Plenu	m		Full	. Plenum	1		1	Evacuated	Plenum		1	ull	Plenu	m
		Wt. No.	Wt.(g)			W	t. No.	Wt.(g)			Wt. No.	Wt.(g)			Wt	. No.	Wt.(g)
				Filling N	<u>lo. 1</u>							1	Filling No	. 4			
6 Mar	74	1	77.592	8	Mar	74	1	102.458	14 Mar	74	1	77.588	14 M	lar 7	4	1	102.453
		2	77.592				2	102.456			2	77.588				2	102.454
		3	77.592				3	102.456			3	77.588				3	102.454
	Av	erage =	77.592			Av	erage =	102.457			Average =	77.588			Aver	age =	102.454
			Wt.	Mercury =	24.86	51 g*						Wt. 1	Mercury =	24.8	52 g*		
				Filling N	io. 2							1	Filling No	. 5			
11 Mar	74	1	77.589	12	Mar	74	1	102.459	15 Mar	74	1	77.590	15 M	lar 7	4	1	102.455
		2	77.589				2	102.460			2	77.591				2	102.456
		3	77.589				3	102.459			3	77.592				3	102.457
	Av	erage =	77.589			Av	erage =	102.459			Average =	77.591			Aver	age =	102.456
			Wt.	Mercury =	24.80	56 g*	•					Wt. I	Mercury =	24.8	61 g*		
				Filling-N	lo. 3												
13 Mar	74	1	77.597	14	Mar	74	1	102,463									
		2	77.596				2	102.464									•
		3	77.595				3	102.463									
	Av	erage =	77.596			A	verage =	= 102.463									
			Wt.	Mercury =	24.8	63 g*	ł										

* Buoyancy correction for weights = -0.004 g added to weight of mercury.

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Plenum No. P-6

		E	vacua	ted Pl	enun	1		Ful	1 Plenu	m			Evacuated	Plenum			Full	l Plenu	m
			Wt. No	o. Wt.	(g)				Wt. No.	Wt.(g)			Wt. No.	Wt.(g)			1	Wt. No.	Wt.(g)
						Filling	No. 1							F	illing	No. 4			
28	Feb	74	1	58.	549		1 Mar	74	1	86.239	11	Mar 74	. 1	58.645	1:	2 Mar	74	1	86.231
			2	58.	550				2	86.238			2	58.644				2	86.231
			3	58.	650				3	86.238			3	58.644				3	86,.233
•		Av	erage	= 58.	650			A	verage	= 86.238			Average =	58.644			Av	erage =	86.232
				W	t. M	fercury	= 27.5	84 g	*				1	Wt. M	lercury	= 27.	584	g*	
			1			Filling	No. 2							F	illing	No. 5			
4	Mar	74	1	58.	552		5 Mar	74	1	86.233	13	Mar 74	1	58.644	1	4 Mar	74	1	86.227
			2	58.	651				2	86.232			2	58.643				2	. 86.225
			3	58.	650				3	86.232			3	58.643				3	86.226
		Av	erage	= 58.	651			A	verage	= 86.232			Average =	58.643			Av	erage =	86.226
				W	t. 1	fercury .	= 27.5	77 g	*					Wt. M	fercury	= 27.	579	g*	
	**		- ,			Filling	No. 3												
7	Mar	74	1	58.	643		8 Mar	74	1	86.230									
			2	58.	642				2	86.232									
			3	58.	644				3	86.232									
		Av	erage	= 58.	643			A	verage	= 86.231									
				W	t. 1	fercury	= 27.5	84 g	*										

* Buoyancy correction for weights = -0.004 g added to weight of mercury.

Plenum No. P-7

		E	vacuate	d Plenu	m	Ful	ll Plenum	1			Evacuated	Plenum	Fu	11 Plenur	n .
			Wt. No.	Wt.(g)			Wt. No.	Wt.(g)			Wt. No.	Wt.(g)		Wt. No.	Wt.(g)
					Filling No.	1						<u>F</u> :	illing No. 4		
28	Feb	74	1	57.838	1 Ma	r 74	1	88.630	11 M	far 74	1	57.830	12 Mar 74	1	88.622
			2	57.838			2	88.630			2	57.830		2	88.622
			3	57.838			3	88.631			3	57.830		3	88.622
		Av	erage =	57.838		1	Average =	88.630			Average =	57.830	1	verage =	88.622
•				Wt. 1	Mercury = 30 .	787 8	g*					Wt. M	ercury = 30.787	g*	
					Filling No.	2 .						F	illing No. 5		
28	Feb	74	1	57.837	5 Ma	r 74	1	88.624	13 M	far 74	1	57.834	14 Mar 74	1	88.623
			2	57.835			2	88.623			2	57.835		2	88.623
			3	57.835			3	88.623			3	57.834		3	88.623
		Av	erage =	57.836		1	Average =	88.623			Average =	57.834	1	verage =	88.623
				Wt.	Mercury = 30.	782	g*					Wt. M	ercury = 30.784	+ g*	
					Filling No.	3									
7	Mar	74	1	57.832	8 Ma	r 74	1	88.624							
			2	57.831			2	88.623							
			3	57.832			3	88.624							
		Av	erage =	57.832			Average =	88.624							
				Wt.	Mercury = 30.	787	g*								

* Buoyancy correction for weights = -0.005 g added to weight of mercury.

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TABLE	4.	Plenum	Volumes
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Date	Book	Page No.	Wt. of Hg (g) $\sigma(g)$	Hg temp. (°C)	Density of Hg (g/ml)	Density of Hg (g/cc)	Plenum Volume (cc)	
			Pler	um No. P-1				
1 Mar 74	1	146	17.573 .001 .	21.2	13.5433	13.5429	1.2976	
5 Mar 74	1	147	17.573 .001	21.9	13.5416	13.5412	1.2977	
8 & Mar 74	1	148	17.577 .001	21.1	13.5436	13.5432	1.2978	and the second
11 Mar 74	1	149	17.577 .001	20.9	13.5440	13.5436	1.2978	
13 Mar 74	1	150	17.577 .001	22.0	13.5413	13.5409	1.2981	
			17.5754 1/80 522,0022 Pler	num No. P-2	A	verage volume	= 1.2978 cc = ,00008	si 1/7250.0002
1 Man 28 Feb 74	2	2	19.799 .001	21.2	13.5433	13.5429	1,4619	
5 K Mar 74	2	3	19.796 .001	21.9	13.5416	13.5412	1.4619	
8 7 Mar 74	2	3	19.799 .001	21.1	13.5436	13.5432	1.4619	
17 11 Mar 74	2	4	19.800 .001	20.9	13.5440	13.5436	1.4619	
13 Mar 74	2	4	19.794 .001	22.0	13.5413	13.5409	1.4618	· · · · · · · · · · · · · · · · · · ·
			19.7976 11.	7900	l	Average volume	= 1.4619 cc ³	5; = 1/36 500 .00 Doy

*Obtained from linear interpolation of tabulated densities (Handbook of Chemistry and Physics, 43rd Edition, page 2157, Chemical Rubber Publishing Co., 1962).

+Equal to density in g/ml + 1.000027.

for solution balance given.

TABLE 4. Plenum Volumes

Date	Book No.	Page No.	Wt. of Hg (g) $\sigma(g)^{\dagger}$	Hg temp. (°C)	Density of Hg (g/-	Density of Hg (g/cc)	Plenum Volume (cc)	
			Plenum	No. P-3				
1 Man 28 Feb 74	2	7	22.155 .001	21.2	13.5433	13.5429	1.6359	
SK Mar 74	2	8	22.156 .001	21.9	13.5416	13.5412	1.6362	
8 Mar 74	2	8	22.155 .001	21.1	13.5436	13.5432	1.6359	
12 Mar 74	2	9	22.155 .001	20.91	13.5440	13.5436	1.6358	
13 Mar 74	2	9	22.153 .001	22.0	13.5413	13.5409	1:6360	
			22.1548 1/20 Si0011 1/20 Plenum	No. P-4		Average volume	= 1.6360 cc	Si= 1/10 400 .000 2
26 Feb 74	2	11	23.646 .001	20.2	13.5457	13.5453	1.7457	
1 Mar 74	2	11	23.640 .001	21.2	13.5433	13.5429	1.7456	
5 # Mar 74	2	12	23.637 .001	21.9	13.5416	13.5412	1.7456	
8 Mar 74	2	12	23.644 .001	21.1	13.5436	13.5432	1.7458	
12 Mar 74	2	13	23.646 .001	20.9	13.5440	13.5436	1.7459	
			23.6426 15	900		Average volume	= 1.7457 cc = ,00006	Si= 1/13,000

*Obtained from linear interpolation of tabulated densities (Handbook of Chemistry and Physics, 43rd Edition, page 2157, Chemical Rubber Publishing Co., 1962).

+Equal to density in g/ml + 1.000027.

 $\frac{1}{\sigma}$ universal for solution balance given.

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TABLE 4. Plenum Volumes

	Date	2	Book	Page No.	Wt. of Hg (g) σ(g)	Hg temp.	Density of Hg (g/ml)	Density of Hg (g/cc)	Plenum Volume (cc)	
					Plenum	<u>No. P-5</u>		1 L		
8	Mar	74	2	17	24.861 .00	01 21.1	13.5436	13.5432	1.8357	
12	Mar	74	2	18	24.866 .00	01 20.9	13.5440	13.5436	1.8360	
14	Mar	74	2	18	24.863 .00	01 22.0	13.5413	13.5409	1.8361	
14	Mar	74	2	19	24.862 .00	01 21.6	13.5423	13.5419	1.8359	
15	Mar	74	2	19	24.861 .00	01 21.9	13.5416	13.5412	1.8360	
					24, 8626 1 2:= .0021	14,800		Average volume	= 1.8359 cc^3	Si= 1/11 700
					Plenum	n No. P-6				
1	Mar	74	2	21	27.584 .00	01 21.1	13.5433	13.5429	2.0368	and the second
5	Mar	74	2	22	27.577 .00	01 21.9	13.5416	13.5412	2.0365	
8	Mar	74	2	22	27.584 .00	01 21.1	13.5436	13.5432	2.0367	
12	Mar	74	2	23.	27.584 .00	20.9	13.5440	13.5436	2.0367	
14	Mar	74	2	23	27.579 .00	01 22.0	13.5413	13.5409	2.0367	
					27.5816	18100		Average volume	= 2.0367 cc = 00005	1/18200
A										

Obtained from linear interpolation of tabulated densities (Handbook of Chemistry and Physics, 43 Edition, page 2157, Chemical Rubber Publishing Co., 1962).

+Equal to density in g/ml + 1.000027.

to universal for solution balance given.

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TABLE 4. Plenum Volumes

Date	Book No.	Page No.	Wt. of Hg temp. Hg (g) $\sigma(g)^{\ddagger}$ (°C)	Density of Hg (g/ml)	Density of Hg (g/cc)	Plenum Volume (cc)
1Moneto?			Plenum No. P-7			
28 Mar 74	2	26	30.787 .001 21.2	13.5433	13.5429	2.2733
5 Mar 74	2	27	30.782 .001 21.9	13.5416	13.5412	2.2732
8 Mar 74	2	27	30.787 .001 21.1	13.5436	13.5432	2.2732
12 Mar 74	2	28	30.787 .001 20.9	13.5440	13.5436	2.2732
14 Mar 74	2	28	30.784 .001 22.0	13.5413	13.5409	2.2734
			307854 1/13460 8:=.0023	. A	verage volume	= 2.2733 (= ,00004

 $\sigma_{universal}$ of balance (based on 261 weighings, 87 averages) = 0.73 mg. $\sigma_{universal}$ of weights of Hg (difference between empty and full plenums) = 0.73 $\sqrt{2}$ mg = 1.0324 mg.

 $\sigma_{\text{universal}}$ of individual vial volume determinations $\approx \frac{1.0324}{13.54} \cdot 10^{-3}$ cc = 0.000076 cc. $\sigma_{\text{universal}}$ of individual volume determination (based on 35 fillings, 7 averages) = .000135 cc.

 $\sigma_{universal}$ of volume due to repetitive fillings with mercury = .000112 cc.

*Obtained from linear interpolation of tabulated densities (Handbook of Chemistry and Physics, 43rd Edition, page 2157, Chemical Rubber Publishing Co., 1962).

⁺Equal to density of g/ml + 1.000027.

[†]σ_{universal} for solution balance given.

cc si= 1/25 400 ,0000g

TABLE 5. Uncertainties in Weight and Volume Measurements

Vessel Type	σ _{universal} Individual <u>Weighings</u>	σ <mark>universal</mark> Weights of <u>Liquid</u>	^o universal Volume due to <u>Weighings</u>	Uncertainty in Mean Volume due to <u>Weighings</u>	Relative' Uncertainty in Mean Volume due to <u>Weighings</u>
Flask	0.45g	0.64g	0.64cc	0.21cc*	4.0.10 ⁻⁵
Plenum	0.73mg	1/03mg	0.76·10 ⁻⁴ cc	$0.44 \cdot 10^{-4} cc^{\dagger}$	2.2.10 ⁻⁵

- * For flasks weighed nine times.
- † All plenums were weighed three times.
- + Flask volume was taken as 5300 cc and plenum volume was taken as 2 cc for relative error calculations.

TABLE 5. Uncertainties in Weight and Volume Measurements

Vessel Type	σ <mark>universal</mark> Volume due to <u>Filling</u>	Uncertainty in Mean Volume due to <u>Filling</u>	Relative [‡] Uncertainty in Mean Volume due to <u>Filling</u>	^o universal Volume <u>Total</u>	Uncertainty in Mean Volume <u>Total</u>	Relative [†] Uncertainty in Mean Volume <u>Total</u>
Flask	0.37cc	0.26cc**	5.0.10-5	0.74cc	0.52cc**	1.0.10-4
Plenum	1.12.10 ⁻⁴ cc	0.50·10 ⁻⁴ cc [†]	2.5.10 ⁻⁵	1.35.10 ⁻⁴ cc	0.60·10 ⁻⁴ cc ^{††}	3.0.10 ⁻⁵

- * All plenums were weighed three times.
- ** For flasks filled twice during volume calibration.
- tt All plenums were filled five times during volume calibration.
- + Flask volume was taken as 5300 cc and plenum volume was taken as 2 cc for relative error calculations.

TABLE 6. Calibration of Mettler PllN

Single-Pan Analytical Balance

1 Kg Wt.		2 Kg Wt.		2826.8 g Bottle Hg		2826.8 g (Wts. + Bottle Hg)	
Wt. No.	Wt.(g)	Wt. No.	Wt.(g)	Wt. No.	Wt.(g)	Wt. No.	Wt.(g)
1	999.8	1	2000.1	1	.2827.1	1	6827.2
2	998.5*	2	2000.1	2	2827.0	2	6827.0
3	1000.0	3	2000.1	3	2826.9	3	6827.1
4	998.9*	4	1998.2*	4	2827.0*	4	6826.7*
5	1000.2	5	1997.0 (19	99.3)*5	2825.5*	5	6826.1 (6827.0)*
6	998.1*	6	1998.9*		2824.6 (2	826.2)*6	6824.7 (6826.3)*

* Settled slowly onto the pan.

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Numbers in parentheses were obtained by tapping the side of the balance while the weights were still on the pan.